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- (54) LUBRICANT-IMPREGNATED FIBERS AND PROCESSES FOR PREPARATION THEREOF
 Mit Gleitmittel Imprägnierte Fasern und Verfahren zu deren Herstellung
 FIBRES IMPREGNEES DE LUBRIFIANT ET PROCEDE DE PREPARATION
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- (73) Proprietor: EASTMAN CHEMICAL COMPANY Kingsport, TN 37660 (US)
- (72) Inventors:
 - NEAL, Richard, D. Kingsport, TN 37660 (US)

- BAGRODIA, Shiram
- Kingsport, TN 37660 (US)
- TRENT, Lewis, C. Johnson City, TN 37602 (US)
- POLLOCK, Mark, A.
 Johnson City, TN 37602 (US)
- (74) Representative:
 Wibbelmann, Jobst, Dr., Dipl.-Chem. et al
 Wuesthoff & Wuesthoff,
 Patent- und Rechtsanwälte,
 Schweigerstrasse 2
 D-81541 München (DE)
- (56) References cited: AU-A- 5 117 264

FR-A- 2 398 832

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Description

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Field of the Invention

This invention relates to the preparation of fibers having lubricant-impregnated surfaces which have improved properties related to overall performance including fiber opening, cohesion, processability and liquid-transport. This invention also relates to novel fiber fulbricants.

Background of the Invention

Fibers for norwowen or faxtile materials must have certain characteristics in order to be considered useful or desirablo. Important performance characteristics to consider in solecting a fiber or fibers for a wide range of norworen, knitted and woven products include the following: (1) fiber processability on norwoven and textile equipment (efficiency, cost effectiveness); (2) fiber/fabric/material*pand* and overall aesthetics when viewed, fouched: used or worn (abrasiveness, softness, fiber-ovening power, openity conflict, offsee, appearance, perception of suitability); (3) stength (4) abhasion resistance; and (5) when applicable, liquid-transport characteristics (wetting, wicking, absorption, liquid-transport durahibit).

Norwoven materials are manufactured by means other than weaving and knitting. The terms "norwoven" and "nonwoven fabric" are general descriptive terms for a broad range of products, such as absorbent pads, wiping/cleaning wabs or labrics, insulation, airomafilation materials, liners, wicks, relatively thick battings, compressed bonded battings or webs, bendages, inconlinence situations, littlers and many other products, inferest in nonwoven materials is enhanced by the fact that such materials can be mass produced efficiently and a frelatively low cost to satisfy many important consumer and industrial needs. Improvements in man-made libers have contributed to the development of the norwoven industry.

Man-made materials have become increasingly plentiful and inexpensive. However in cortain characteristics many of these materials do not compare well to natural fibers such as in the ability to transport moisture satisfactority. Several methods have been devised to improve the characteristics of man-made materials, such as polyester. Io more closely resemble natural fibers such as cotton. FFA-2.998-322 discloses inishes that can be applied to fibers such as in a bath. US. Patarita. Sol. 90.402, 2731-242, 2828-528 and 4.000,044 and this outmaried objective foreign such as hardward as foreign and softeness. US. 4.374,950 discloses the production of polyester fibers of improve certain properties such as hardward softeness. US. 4.374,950 discloses the production of polyester fibers of improved statishility that are made by mixing the polyester and an end-capping reagent prior to fiber formation. EP 0,188.091 discloses the production of a highly absorbant nonward web by costing the web with super-absorbant-polymeric particles. US. 4.482.792 discloses fibers of improved cover, softness and wetting her work with super-absorbant polymeric particles. US. 4.482.792 discloses fibers of improved cover, softness and wetting her work with super-absorbant polymeric particles. US. 4.482.792 discloses fibers of improved cover, softness and wetting hardwards that is the control of the control of

All of these various advormentioned characteristics are important; however, unlike fabrics, steple fibers must also be satisfactorly processable in an economical manner under conventional production conditions by the equipment used in nonwoven and textile manufacture. Staple fibers are cut into suitable lengths (usually about 1 to 10 cm) for processing in a manner similar to natural staple fibers, such as cotton, in both textile and nonwoven machinery. These fibers must perform satisfactorily in such known operations as opening, blending, lededing, carding, bonding, healing corpressing, cooling, hydro-entangling, needle-punching, drawing, roving, spinning, knitting, weaving, and others as selected for the various pornover or textile materials.

Crimping of staple fiber by various means has been found to be an essential element in producing a certain controlled amount of fiber cohesion or resistance to pulling apart in forming carded webs. These webs of 'opened' (separated) these are formed in flat-top or roller-top carding machines or the like as part of nonwowen or textile processos.

Poor crimp formation, especially in filters with non-round cross-sections, has been associated with low and variable ochesion, weak whee, web separation, and poor processability during carding and/or subsequent operations. Relatively high tubricant levels (applied at room temperature), particularly above about 0.2 weight percent, of contain processing ultricants can cause unsatisfactory cohesion and processability problems in carding, etc. When such high levels of these lubricants are applied prior to the crimper (such as by conventional kiss rolls), low fiber-to-metal friedom within the crimping chamber interferes with the capability to produce normal crimp frequency (crimps per nich) with sufficiently low foreover, and crimp and crimp

Two types of commonly used processing lubricants are based on potassium launyl phosphate or mineral oil with the addition of antistate agents, friction modifiers, etc. as needed. A high level (above 0.2 to 2. ut % or greated) these and many other lubricants applied prior to the crimper using prior art methods (usually lubricant coated, rotating, contract loss at approximately room temperature located remote from the crimper input) can have an adverse effect on crimp formation and/or tend to cause problems in carding by poor cohesion and/or by building up relatively quickly a detrimental coating on the carding with endfor other problems. Additionally, these builtvasted to on the vay coad hydrodynilic action.

Additionally for certain applications, liquid-transport durability is a desirable characteristic but difficult to obtain in some man-made fibers, partial man-made fibers, partial microlarly those with suitable non-nound cross-sections. have some initial liquid-transport characteristics. However, after wet usage, weeking or securing, the ability of those fibers to transport characteristics. Adminish similification is some instances deminish similification.

Any method of improving any of the aforementioned characteristics without significant adverse affects on other characteristics would be very desirable.

Derwent Abstract No. 84-018167 referring to EP-A-0 098 477 discloses a process for preparing filaments and fibres made of acrylonitrile polymers which contain at least 40% by weight of acrylonitrile units in a continuous operation by spinning a spinning solution of the polymer into a spinning cell, evaporating at least some of the spinning solvent in the spinning cell, spinfinishing, stretching, crimping, heat-setting and, if desired, cutting.

Derwent Abstract No. 79-64196B discloses finishes for synthetic fibres, in particular polyester reinforcing yarn containing polysiloxane, copolymer of ethylene oxide and dimethylsiloxane, polyethylenimine etc.

20 Summary of the Invention

The present invention is directed to fibers having improved opening characteristics, cohesion, processability, hand, and/or liquid-transport properties in which a significant amount of a lubricant is adhered to the surfaces of the fibers

These improved libers are made by the process as defined in claims 1 - 10 and comprising spreading at an elevated temperature onto the filbers a substantially non-flacky wettable lubricant as a mixture, emulsion or solution in water, followed by a pressure application means and subsequently healing the filbers at an elevated temperature for time sufficient to dry or bake the lubricant onto or into the surface of the filbers. Filbers made by this process are particularly useful in making nonvoven materials.

Another aspect of this invention entails novel fiber processing lubricants as defined in claims 11 - 19 and comprising a mixture of high and low molecular weight polyethylene glycol fattly acid selsers preferably in combination with a minor amount of a suitable antistatic agent. In some applications, this novel lubricant or mixture can be applied to the fibers of choice at about room temperature by various means as a less preferred option.

Yet another aspect of this invention entails a novel hydrophilic processing lubricant for use with fibers, particularly bilder fibers, comprising a mixture of a suitable sinitiated agent and at least one polybethylene glycon monoslaurate or monoslaurate browning a sorbitan group such as polyethylene glycol 880 sorbitan monoslaurate and/or polyethylene glycol 880 sorbitan monoslaurate and/or polyethylene glycol 880 sorbitan monoslaurate.

Brief Description of Drawings

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Fig. 1 - Schematic flow chart of a preferred tow-processing operation within the scope of the present invention. The solution of heated processing lubrocant is preferably applied by at least one jet immediately prior to the crimper. At least one component of a lubricant and/or a cross-linking agent can be applied prior to the heat-setting unit.

Fig 2 - Schematic representation of examples of fiber cross-sections of preferred non-round spun fibers having a plurality of goones. Figure 2s is a representation of a more preferred cross-section with two grooves and is particularly useful for deniers less than about 5.0 (5.6 decitex), L1 is a major axis; L2 is a minor axis. W is the width of the groove; thicker lines represent the surfaces outside the groover, thicker lines represent the surfaces outside the groover. Figure 26 illustrates a cross-section which has four grooves. Figure 26 illustrates a cross-section which has four grooves. Figure 26 represents the general form of a much preferred eight-groove cross-section which is useful for deniers greater than about 5.6.8 deciteds.

Fig. 3 - Graph of the wettability (vertical-wicking performance) of Samples A, B, C. and D from Example 5. This graph illustrates the amount of water in grams transported over time in seconds.

Fig. 4 - Detail of a most preferred method of applying the hot solution of processing lubricant to the fibers of a tow prior to crimping. The crimper is a stuffer-box type crimper with advancing rollers or can be any suitable type of crimper.

Fig. 5 - Graph representing the drop-wetting time in seconds of various nonwoven fabrics made from the various fiber samples as described in Example 2

Fig. 6 - Schematic flow chart of a most preferred tow processing operation within the scope of the present invention. Excess fliquid is removed by at least a Partial Liquid Fernoval Means 1 following both the drafting bath and the neutralization bath and the low is sufficiently dried prior to being contacted by the heated solution of processing bibricant parties.

immediately prior to crimping. Additional or alternate processing-lubricant application means, treatment, and/or neutralization means are illustrated at 2A. If an additional means is utilized at 2A, then the tow is substantially dried prior to being contacted by the heated solution of processing lubricant at 2B. Squeeze rolls are shown at the input to the 4th set of rolls.

Detailed Description of the Invention

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Fiber produced according to the process of the present invention, particularly those having at least one continuous growe, having either round or non-round, are characterized by an unexpected combination of deserable proporties including fiber opening, card-web quality, ochseiveness, good textile and nonwoven processability, hand, and bonding properties. In addition the liquid-transport capabilities are at least as good as and in some instance possibly better than those of companishe libraries that are not treated according to the process of the present invention. The liquid-transport capability is more durable in that, after vigorous socuring such as with hot water for many seconds as later described, these treated fibers and products made therefore (at least when causits treated) unexpectedly (1) retain effective amounts of contain fubricants and (2) more importantly, provide greater liquid-transport durability than comparable non-freated fibers/products.

In particular, these novel fibers can be efficiently conducted through nonwoven processes with subsequent bonding and/or calendering processes, as appropriate to provide hydrophilic fabrics which have excellent cover, softness hand and/or overall properties compared to untreated fiber.

If desired, the process of the present invention also eliminates the need for steam application prior to the crimper; however, steam heating is a viable, yet less desirable, option for heating the novel lubricant mixture.

Any method of applying the processing lubricant to sufficiently coat the fibers, including the grooves, that also softens the fibers just prior to the crimper is envisioned to be within the scope of the present invention.

A preferred process of the present invention and falling under the definitions of claim 1 comprises:

(A) contacting at an elevated temperature at least one tiber with a sufficient amount of a solution containing a

(x) contacting at an elevated companies at pass one likely with a sense of a solution of a solution contacting a sufficient amount of at least one substantially non-static hydrophilic (wettable) processing lubricant to coat said fiber;

(B) crimping at an elevated temperature the lubricant-coated fiber of (A); and

(C) heating the thus crimped lubricant-coated fiber of (B) at a sufficient temperature for a sufficient time to dry or bake said lubricant onto and/or into the surface of said fiber.

A more preferred process of the present invention and falling under the definitions of claim 1 comprises:

(A) coaling at least one caustic-treated non-round fibor with at least about 0.1 weight % and most proferably at least about 0.3 weight % of at least one substantially non-tacky, wettable, processing lubricant with antistatic properties at a temperature between about 40°C and the boiling point of the lubricant to cost said fibor.

(B) crimping at an elevated temperature the lubricant-coated fiber of (A); and

(C) heating the thus crimped lubricant-coated fiber of (B) at a temperature between 40 and 180°C for sufficient time to dry or bake the lubricant onto and/or into the surface of said fiber.

The mixture, solution or emulsion of processing lubricant preferably contains at least about 5 vt. % processing ubricant, more preferably at least about 10 vt. % with about 20 vt. % being most preferred. The solution should be relatively free-flowing in that when heated to at least 40°C it can spread and flow readily when it is placed on a glass surface angled at 30° from horizontal. To avoid being too viscous the solution preferably contains less than about 40 vt. % slubroant more oreferably best han about 40 vt. % slubroant more oreferably best han about 50 vt. %

The resulting novel fibers are preferably coated with at least 0.1 wt. % lubricant based on the total wt. % of the fiber and lubricant and more preferably at least about 0.2 wt. % lubricant with at least about 0.3 to 3 wt. % lubricant being most preferable.

Not all lubricants are suitable for use in the present invention. We have found that commonly-used processing lubricants, such as potassium laury phosphate and minised oil types even applied according to the process of the present invention, all low and particularly high levels, are not suitable for use with liquid transport fibers, particularly the caustic-treated non-round fibers described hereinafter. It is believed that the unsuitability of these lubricants is due to their relative hydrophoch enture. In addition, however, not all hydrophile ubricants are suitable. Suitable hydrophile lubricants must also create at least a contain minimum level of cohesion or fiber-to-fiber friction without being excessively "tacky" or "sticky" when drid as a hieronizater described.

The processing lubricant must be substantially non-tacky when dried. In other words, when the lubricant is coated and dried on a surface, that coated surface should not easily adhere or "stick" to other non-tacky surfaces. The fibers

coated with the dried-on or baked-on non-tacky lubricant should not be sticky and should be cardable and capable of being efficiently separated (opened). These fibers should card without wrapping, or "loading" the main carding cylinder or other cardino components and should produce acrided whose which have sufficient strongth for subsecuent operations.

The processing lubricant should also act as a surfactant and be wetfable or somewhat hydrophilic and mix with solutions, emulsions or mixtures containing hot water although the processing lubricant could, if desired, be applied to fibers in a non-aqueous solution. When this lubricant is dried on a surface, such as a thin fill not plastic, it is should spread or disperse water droplets that louch the surface. This processing lubricant should enhance the liquid-transport properties of a fiber, once it is dried or belace not an admir into the surface of the fiber.

Additionally, the processing lubricant should be of a substantially low-static nature and/or allow for at least satisfactory control of static. This lubricant should control static either alone or in the presence of a minor amount of at least one antistatic agent.

Antistatic agents useful in the present invention include quaternary amine salts, salts of polycoxyothylone morganic tatly alcohol esters, effootilate salts of quaternary ammonium compounds, etc. The preferred antistatic agents are the salts of quaternary ammonium compounds including the effootilate salts and acid salts such as the acetales, lactates, and proporates with the othosultate salts being more preferred. The most preferred dehoustlate salts and exclusional salts and exc

The processing lubricant of the present invention is preferably at least partially water soluble and is not too viscous when in solution with water under the conditions when applied to the fibers. The lubricant of the present invention can contain a major portion of a polycoxylthylene fally acid ester such as a methyl-capped polycoxylthylene laterate, a poly-eithylene glycol further, or a fatty and glycerful such as a glyceryl cleant. The processing lubricant of the present invention can aske contain an amount of a competible surfacettal native softening agent. By competible it is meant that this component would not cause an adverse reaction such as getting, coagulation, precipitation, etc.

The processing lubricant is preferably selected from (A) a mixture of a major amount of a methyl-capped polyoxyethylene (x) fatty sets (x) represents about 2 to 50 moles of ethylene oxide and the latty seter contains 7 to 18 carbon atoms such as laurate), and a minro portion of qualemany amine carbonate or often suitable antistatic agent, and (B) a mixture of a major portion of at least one polyethylene glycol mono or dilaurate (molecular weight between about 90 and 2,000 with 400-600 being more preferred) and, if needed, a minor amount of a suitable antistatic agent with the mixture (B) being the most preferred processing between

The mixture (A) preferably contains about 55 to 80 % by wt. of a methyl-capped polyoxyethylene (x) laurate wherein x represents about 2 to 50 moles of ethylene oxide.

According to another aspect of the present invention, an improved lubricant mixture is provided that generally falls within (B) above containing low and high melecular weight polyethylene glycol falty acid seters such as polyethylene glycol 400 monolautae and polyethylene glycol 600 monolautae to an importance and suitable antistatic agent, such as 4-ethyl, 4-etbyl, morpholinum ethosullate. By definition, a low molecular weight polyethylene glycol falty acid eater has a molecular weight in the polyethylene glycol portion below 500. By definition, a high molecular weight polyethylene glycol portion below 500. By definition, a high molecular weight polyethylene glycol portion above 500. The most preferred high molecular weight polyethylene glycol falty acid ester is polyethylene glycol 400 monolaurate and the most preferred high molecular weight polyethylene glycol falty acid ester is polyethylene glycol 600 monolaurate. This novel lubricant mixture is much preferred for use in the present invention and preferably comprises a major portion of substantially equal portions of the low molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular weight polyethylene glycol falty acid ester and the high molecular w

The novel lubricant mixture most preferably contains at least about 40 weight percent of the low molecular weight polyethylene glycof latty acid sets rat least about 40 weight percent of the high molecular weight polyethylene glycof latty acid ester and about 20 lot 1 weight). So a suitable antistatic agent with 4-ethyl, 4-echyl, morpholinium ethosulfate being the preferred antistatic agent.

Other preferred lubricants, particularly for use with binder fibers, include a major portion of at least one polyethylene glycol monolaurate or monostearate having a sorbitan group such as polyethylene glycol 880 sorbitan monolaurate and/or polyethylene glycol 880 sorbitan monostearate mixed in water with a minor portion of a suitable antistat. This novel lubricant most preferably contains (excluding water) at least about 80 weight % polyethylene glycol 880 sorbitan monostearate and/or polyethylene glycol 880 sorbitan monostearate and/or polyethylene glycol 880 sorbitan monostearate and polyethylene glycol 880 sorbitan monostearate and about 1 to 20 weight % of a suitable antistat with 4-ethyl. 4-etyl, morpholinium ethosultate being most preferred.

A binder fiber is a material substantially in fiber form, such as crimped staple which is blended as a minor component with a more stable, heat-resistant major component fiber, which can be heated and compressed to form a bonded nonworm fabric.

The solution of lubricant can, if found to be appropriate for a particular need, contain minor amounts of at least one other additive, such as a coloring agent, aroma-enhancing agent, scouring agent, anti-fungal or anti-bacterial agent,

edecamer additional antistatic agents, other hydrophile components, a finction-modifying agent, a super-absorbent powder or polymer (Increescent additive, antiseptic additive, additives suitable for comenie purposes, althoystized olivyl aicohol (cosentic grade, etc.). Such other additive can be applied, as an option, to the tinal nonwoven or textile product. As appropriate and feasible, suitable components of our novel lubricants can be modified, such as by methyl-capping, etc. The processing lubricant can, if applied in a separate step, contain a cross-linking agent with or without a catalyst and/or additives which have bonding properties. An example of a suitable cross-linking agent is "LUREEN 2185" a hydrophobic cross-linking silicone from G. A. Goulston Co. Examples of suitable informor-modifying agents are a polycovyethylene-polycoxyprocylene condensate, such as Pluracol V-10 and various fatty acid (C10-C18) diethanolamide condensates, such a smade by Emmy Chemical Co.

The processing lubricant can also contain minor or trace amounts of additives useful in the processing of fibers such as spinning lubricant, polymer, chemicals useful in dyeing, etc. and mixtures thereof.

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The processing-lubricant solution solvent is preferably selected from the group consisting of water, water containing a minor amount of acetone, ethanol or other solvents, water containing minor amounts of reaction products or materials washed from the fiber, etc. and mixtures thereof with plain or distilled water being more preferred.

Although the present invention is an improvement over the art, not all lubricants, including the novel lubricants, perform equally well on all fibers. The most preferred suitability must be determined on a case-by-case basis matching fiber and specific lubricant.

Additionally, the novel lubricants can be applied as appropriate to plastic tapes, ribbons, films and other manufactured articles

Prior to the application of the fubricant the fibers of the present invention are preferably causalts treated, such as by a causalt is obution at an appropriate concentration followed by neutralization. This causalt treatment is most preferably conducted prior to application of the hot processing lubricant solution as shown in Figure 1 and 6. This causalt treatment is preferably conducted by the following steps: (1) causalts treating the fiber, (2) heating the fiber, and (3) substantially conducted at a temperature of all least about 150°C, more preferably at a temperature of all least about 150°C, more preferably at a temperature of all least about 145°C for approximately 2 to about 25 seconds. Of course, this temperature should not be so high a to be mat the fiber or degrade the lubricant. The suitable acid used in the neutralizing step is preferably selected from the group consisting of acetic acid, citric acid, ascorbic acid, and/or mixtures thereof. The process of the present invention in combination with this causalts treatment or surface hydrolyse results in novel fibers which have unexpectedly a superior combination of important characteristics including processability liquid-transport, and/or overall performance compared to other fibers not treated by causalty and an appropriate amount of the novel horburbricant protor to crimpion.

The present invention is most preferably directed to caustic-treated and neutralized fibers with suitable non-round cross-sections having longitudinal grows that are substantially continuous in which a significant amount of a hydrochilic processing lubricant is adhered to surfaces of the fibers and a significant amount remains after a hot-water treatment as described. These fibers have improved overall performance including processability. However, the novel process of this invention can be used to improve the crimp formation, ochesion, processability and overall performance of fibers not treated with caustic.

Fibers with many longitudinal or axial grooves land to hold liquid, such as neutralization solution, in the grooves and do not permit sufficient lubricant to enter. Therefore, it is important to remove this excess liquid prior to contacting the fibers with the heated processing lubricant so that the grooves are substantially devoid of liquid. This can be accomplished by a partial or total liquid removal process in which at least one liquid removal means, such as bars, squeezer collers, and/or air jets physically removes a significant portion of the flould. For substantially total liquid removal this physical removal must be followed by drying at elevated temperatures prior to the application of the heated processing lubricant. Figure 1 illustrates the location of Liquid-Removal Means 1 that can be employed following the 1st stage drating bath and/or after the optional neutralization bath to at least partially remove liquid from the tow.

The fiber is contacted with a continuous flow or semicontinuous pulsed flow of the solution of processing lubricant. The deviated temperature, preferably, at a temperature of at least about 40°C up to the boiling point of the solution. This temperature is more preferably between about 50° and 100°C with a temperature less than about 55°C being most preferred. For drawn polyseter this most preferred fromporature is botween about 70° and 55°C. For brinder fibers, such as coordivesters and undrawn polyseters, the referred for moreature is between about 40° and 70°C.

The application of the hot processing-fubricant solution can be conducted in any suitable manner so long as substantial loss of heat is avoided (such as by tine droplet formation) and a sufficient amount of the processing fubricant is coated or the surface of each of the fibers. That amount should preferably be sufficient to maintain satisfactory crimp formation, cohesion and processability. A much preferred process of applying this hot lubricant solution is by the use of one or more jets positioned just prior to crimping such as shown in Figure 4. This figure illustrates the use of both top and bottom jets to facilitate penetration of the hot lubricant into the center of the fiber bundle (low). It is important that, as far as it is practical, hot lubricant contacts each fiber so also heat and soften each fiber. Therefore, during or after contaction of the fiber with the continuous flow of processing fubricant, an elevated formaceafure is maintained as the

lubricant is spread in a substantially uniformly manner onto the fiber. A subsequent crimping or compression means (such as a crimper or compression roll) is the preferred method used to spread the lubricant and press it into the grooves of the fiber. Additionally, thoroughly coating the fibers with the proper lubricant, such as the most preferred of mixture (B) (heated lubricant-mistaft, helps protect the fibers against damage during the crimping process

It is also preferred to spread the lubricant onto the fiber to a certain extent during and/or immediately after application of the lubricant prior to any crimping means. The lubricant can be spread by any conventional means but is preferably spread by a spreader bar, compression rolls, and/or a hot lubricant application jet in the shape of a spreader bar as shown in Figure 4. These spreading means are also preferably vibrated.

To swod soutfring or other derinage to the filtor, the filtor should not contact a dry jet surface. When a jet contacts the filtors, the side or jet holes are most preferably located in a curved contact surface oriented towards the advancing filtor as shown in Figure 4 to minimize dry contact between the tow and the bar in order to prevent exuffing or otherwise dimanging the filtor as lar as practical. Thus, Figure 4 illustrates a novel and much preferred application means for hot lutricant, practically where at least one spreader bar is suitably mounted and equipped with vibration means to facilitate filter separation and lutricant penetration into the tow band to coat the filters more uniformly. As an option, the bottom join or jets can be speaded from the tow and can apply heated fultricant at sufficient pressure to impring eyon the tow. Appropriate supply tank, stirring means, heating means, pumping means, reconstitution means, housing, drains and recirculation vould be provided.

The use of hot-lubricant lets in series prior to the crimper on the tow processing line is illustrated in Figures 4. The tow is maintained under appropriate tension between the last roll and the crimper and, as stated above and illustrated in Figure 4, the slotted let is oriented to prevent contact of the tow with a "dry" (unlubricated) surface (such as metal or ceramic) which could cause damage to the fiber (fused fibers, broken filaments, "skin-backs", etc.). A series of small holes can be substituted for the slot, if desired. The adjustable flanges hold the tow in proper position and cover the slot or holes at the tow edges as required for various tow widths. This bottom jet with either a slot or holes can be constructed with multiple lubricant-supply chambers oriented across the tow band. Figure 4 illustrates the multi-let application means which is a most preferred embodiment of the present invention. In order to provide for adjustment of the % lubricant applied and/or lubricant concentration used for any given fiber type, facilities can be provided to permit each jet to be operated, adjusted or disconnected independently from the others, in a most preferred embodiment, at least one of the two too jets has a common mount and/or support member with at least one of the spreader bars such that the too jet and bar can be pivoted or elevated by any suitable means to provide convenient access to the tow path during start-up when the tow is placed in the crimper rolls. One embodiment of this common mount and/or support member is illustrated in Figure 4 by the broken lines. The first (upstream) jet applies heated lubricant on top of the tow band. The jubricant forms a surprisingly stable, small concentration (bead) at the input side of the first spreader bar. This spreader bar spreads the lubricant from the first jet and causes penetration into the tow, thus increasing the uniformity of lubricant application (a top jet similar in design to the bottom jet could also be used to replace the top jet and/or spreader bar). Lubricant applied by the bottom let is pushed upward into the tow by the rounded top portion of this let. An optional spreader bar (not shown) located beneath the tow can be located downstream from the bottom jet and can have a common mount and/or support member with the bottom jet. The last (downstream) top jet can apply additional jubricant which forms a small bead on top of the tow at the crimper input to be forced into the tow by the crimper rolls. The bottom jet can be operated in combination with one of the top jets. This novel multi-jet lubrication means should be located as close to the crimper input as is practical preferably within about 90 inches (about 229 cm) most preferably within about 60 inches (about 152 cm) of the crimper with the closest jet most preferably located less than about 24 inches (61 cm) from the crimper. It is preferred that the distance from the first jet to the third should not exceed about 6 feet (183 cm). Appropriate insulation can be used to help maintain the lubricant in a heated condition. In addition, the jet(s) can be designed with a novel circulation system (not shown) such that only a portion of the lubricant exits the jet(s) and is being constantly applied to the tow while the remainder of the lubricant is returned to be reheated in the heated supply tank in a semi-closed loop. This recycling of lubricant should help keep the lubricant hot and also avoid plugging of the let. The heated supply tank can be equipped with automatic monitoring and correction systems for lubricant concentration, temperature sensors, insulation, etc. as needed to facilitate uniform application of heated lubricant.

A less preferred ombodiment is similar to Figure 4 except a lubricant-coated, rotating, tow-contact roll which is partially immersed in a bath of heated lubricant is substituted for the bottom slotted jet. This embodiment is much less preferred because it is more complex, would tend to contaminate the lubricant and is more difficult to insulate

A less preferred option is the application of the most preferred lubricant in the neutralization bath followed by a removal means for excess liquid and a heating means prior to the crimper.

An even less preferred option is the application of the most preferred novel lubricant mixture by conventional means followed by a steam chamber to heat the fiber and applied bubicant followed by a termiping and heating in a tow dryer unless contact means, such as spreader bars or rolls are included to increase the penetration of the lubricant into the convoice of the fibers.

Another less preferred option, although an improvement over the art, is the application of a most preferred novel

lubricant after the crimper and tow dryer in the conventional manner. However, the opportunities to force heated lubricant onto and into the grooves of the filters, is onlinear crimp formation, and to help protect the filter surfaces during passed through the crimper are lost. It is believed that, if a conventional application of steam is used prior to crimping, the novel lubricant composition even though applied by conventional means, can be used to facilitate, to a certain extent, the processability of the fiber through nonewore of resting machinery and to make some improvement in overall performance. Such conventional application means can include immersion baths, spray-application means (such as by airless jets or air-powered jets, etc.), application opinions with stetle) to achieve the two band. This novel bulbreant composition of carbon, and is not the support of the proposition of the p

According to the process of the present invention, the fibers containing the coating of heated processing lubricant must be treated to a dying sits such as heating in the low dayer. This tow diver should be captiged with an air circulation system. This completes the attachment of the processing lubricant securely to the surface of the fibers, particularly to the surface in the grooves of non-round fibers and more particularly causatic-treated grooves. The overall heating or drying time is preferably best twan about a familiae. This dying step is preferably conducted at a temperature of all least about 40°C more preferably bestewen 50°C and 115°C for at least about 20 exconds, even more preferably between 50°C and 115°C or at least 100°C and 115°C. For brider (fibers such as copyolevers and underward projecters the temperature is between about 40°C and 10°C. For brider (fibers such as copyolevers and underward projecters the interpreture is between about 40°C and 10°C. For brider (fibers such as copyolevers and underward product, the heat-set cablect can be operated at or near room temperature, if desired, with essentially all of the tow drying treatment being accomplished in the tow dryer.

The thus heated, lubricant-cealed liber, when appropriate, also can be heated a second lime. This second heating temperature is perfearably at least about 10 to 60° to higher than the first tow dyer section. The contacting time for this second heating is at least about 5 seconds. This second heating is preferably conducted at a temperature of at least 135° C for at least about 5 seconds, preferably over 10 seconds with over 20 seconds being most preferred. This second heating or tow drying step can also be conducted at a temperature of at least 175° C for at least about 5 seconds. The heating conditions used should be appropriate for the type of nonwoven or textile processing used and the performance characteristics required for the eventual product.

We believe that most all types of synthetic libers could be benefited, to some extent, by being treated according to the process of the present invention. Examples of suitable fibers that can be treated according to the present invention include those selected from the group consisting of polyseiters including opoplyseters, cellulose accitate, modacrylic, nylon, oellins, viscose rayon, polyphenylene suitide, libers made from biodegradable materials, and suitable mixtures or blends thereof. The preferred fibers that can be treated according to the present invention are polyseiters, cellulose acetate, modacrylic, nylon, and viscose rayon with polyseiters and cellulose acetate being most preferred. The preferred opylesters, including polyseiters are selected from relatively onerated polyseiters, featively uncriented polyseiters, polyseiters containing cellulose acetate, polyseiters containing cellulose acetate, polyseiters on starting cellulose propionate, polyseiters featively material polyseiters, individently and alignative polyseiters befinded with cellulose acetaes. In addition, polyseiters with chive been modified chemically or by a polymerized exterior coating can be benefited by being treated according to the process of the present invention.

The cellulose acetate fibers useful in the present invention are prepared by melt-spinning or conventional solventioning means using acetone as a solvent. The cellulose acetate can contain additives which further enhance hydrophilic action and/or other desired properties.

The polyseter materials useful in the present invention are polyseters or copolyseters that are well known in the art and can be prepared using standard techniques, such as, by polymerizing dicarboxylic acids or esters thereof and glycols. The dicarboxylic acid compounds used in the production of polyseters and copolyseters are well known to those skilled in the art and illustratively include terephthatic acid, isophthatic acid, p.p*diphenyldicarboxylic acid, p.p*dicarboxylic a

Suitable aliphatic glycols for the production of polyesters and copolyesters are the acyclic and alicyclic aliphatic glycols having from 2 to 10 carbon atoms, especially those represented by the general formula HO(CH₂,OH, wherein p is an integer having a value of from 2 to about 10, such as ethylene glycol, trimethylene glycol, tetramethylene glycol, pontamethylene glycol, documentlylene glycol, and the like

Other known suitable aliphatic glycols include, 1.4-cyclohexanedimethanol, 3-ethyl-1.5-pentanediol. 1,4-xylylene, glycol, 2,2.4-4-tetramethyl-1,3-cyclobutanediol, and the like. One can also have present a hydroxylcarboxyl compounds such as 4-hydroxylearboxyl carboxyle

as useful to those skilled in the art.

It is also known that mixtures of the above disarboxylic acid compounds or mixtures of the aliphatic glycols can be used and that a minor amount of the disarboxylic acid component, generally up to about 10 mole percent, can be replaced by other acids or modifiers such as adipic acid, sebacic acid, or the setters thereof, or with modifiers that impart improved dyeability or dyeability with basic dyes to the polymens. In addition one can also include pigments (such as blanc lixe), dedustrants (such as TICs) or optical brightenes by the known procedures and in the home amounts.

The most preferred polymers for use in the present invention are (1) relatively uncriented and relatively oriented poly(ethylen teroprithate) (PET). (2) pophysistors based on poly(ethylen teroprithate) particularly those suitable for use as binder fibers, (3) poly(ethylene terophthate) containing cellulosic additives and/or modified starch, such as starch acotate, and (4) collulose acetatic fibers.

The fibers of the present invention are preferably non-round libers having at least one continuous groove such as toxes disclosed in U.S. 4.942.792, U.S. 4.954.398 and Patent Application 07/33.651. The disclosures of which are incorporated in their entirely hardin by reference. The surface of the groove is most preferably rougher than the surface outside the groove. Examples of various fiber cross socitions are illustrated in Figures 2a, 2b, 2c and 22. Figures 2a and 2d are the more preferred cross sections treated according to the present invention. It is besieved, however, that the overall performance of any non-round liber in crimped staple form will be improved by the process of the present invention. It is besieved, however, that the overall performance of any non-round liber in crimped staple form will be improved by the process of the present invention, and the process of the present invention. It is besieved, however, that the overall performance of any non-round liber in crimped staple form will be improved by the process of the present invention, process and the process and/or channels as shown. The broken lines to the left of 2c are included to illustrate various alternative designs and/or additions to the basic design. The grooves could also be arranged in a circular pattern around a solid or hollow occor. The preferred non-round fiber has at least 1 up to 30 or more grooves a read or channels and/or legs which are substantially continuous. Flosers having a plurially of grooves have a larger surface area per until weight than round fibers and thus can be coated with more bufferiar. These having is control than continuous cross-sectional groove preferably have at least about 0.3 w. % lubicant coated on their surfaces whereas fibers having five or more grooves have at fless the state about 0.3 w. % buffering coated or of their surfaces.

A preferred liber form useful in the process of the present invention is a tow of continuous filaments of between about 10,000 (11,111 decitex) up to at least 100,000 (11,111 decitex) total denier. However, tows of much greater denier can be used also. This tow as with other tows (crimped or non-crimped) can be processed through a tow feeder after the tow dyer (skipping the cuttler) and collected in a baler to form bales which are convenient for shipment. The low subsequently can be opened or spread by rolls and/or jets and threater used in various nonvower products, filters, etc. For staple fibers, the total tow denier can be as small as 30,000 (33,333 decitex) and as large as at least 2,000,000 (2,222,222 decitex). It is also preferred that the fiber of the present invention be subjected to crimping immediately being contacted and spread with the heated solution of processing luteriant. The preferred drimped or non-crimped fiber has a staple length of about 0.5 cm to about 15 cm and/or a denier per filament of about 0.8 to 200 (0.89 to 222 decitex).

The process of the present invention preferably entails contacting a group of ilbers arranged in a relatively flat band (farmy or undrawn two) with at least one of cortain processing lubricants at an elevated temperature, causing the processing lubricant to penetrate into the two to coat the fibers; subsequently subjecting the two to pressure via diviner rolls followed by heating the tow parent processing lubricant on the sufficient to bake or dry said lubricant onto and/or into the surface of the fibers. The driven rolls can be the rolls of a crimory.

The treated fibers in the form of tow crimped staple or uncrimped staple can be subsequently blended or combined with all least one other low or staple fiber (such as a binder fiber); subjected to suitable nonwoven processing to form a wob with the web being subsequently heated and appropriately compressed to cause the blended fibers to compress and bond so as to produce a bonded, nonwoven material, such as a falorit or batting.

A most preferred process of the present invention entalls (1) subjecting a tow of caustic-treated and subsequent-penetralized polypeiser fibers as described to a hearing device, most preferably hotaling heated drums with the vern-perature controls and/or moisture sensors following an at least perial removal of water after the neutralization step and an optional application of at least one higher than the dried tow from the heating device at a tersion suitable for proper crimping, (3) applying at least one heated processing lubricant to the dried tow, (4) crimping the fibers or applying rotating compression rolls to the fibers (preferably immodiately after applying lubricant); and (5) heating the tow at temporature for a time sufficient to bake or of whe bulbers and to and/or not be surface of the fibers.

The temperature range for the towdyer is important with regard to maintaining the desired crimp angle. For example, a tow of crimpod fiber after being dried in the tow dyer for 5 minutes at 75°C could have a well-formed, relatively sharp average crimp angle of about 65 to 60 degrees (by estimation method). However, this same tiber would have successively wider, more open, more rounded, crimp angles, if it had been dried at 155, 150 and 175°C for the same length of time. Assuming no change in hydrophilic lubricant, the increasingly more open crimp angles create an increasing tendency loward reduced fiber cohesiveness. Thus, the obsessiveness required for proper performance of a given their or a particular nonwoven or textile operation must be considered and the temperature of the low dryer is one of the factors which must be taken into account.

The fiber strength (tenacity), fiber elongation, percent shrinkage, etc., required for a particular product must be

considered in determining the temperatures and/or dwell times used before and/or after the crimper.

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It has also been found that cortain amounts of lubricant can be lost during passage through that low dryer and/or bonding oven depending upon temperature and time. Thus the amount of lubricant applied to the liber must be sufficient to compensate for these losses and meet the target level established for the final product, such as a bonded hydrophilic

Overall, it is clear that several factors must be considered in establishing the operating temperatures and wholl times for a given fiber Applying butcheant (particularly the novel hydrophic lubricants) in a heated condition prior to the crimper as described provides an extra margin of safety in terms of crimp formation, particularly with regard to crimp and particularly domation.

Along with the appropriate crimp frequency, the lubricant composition, % bubicant, etc., it is most important to maintain an average crimp angle which provides sufficient filter cohesion for at least satisfactory processing during opening, blonding, carding and subsequent operations. In addition, the crimp apex should be relatively "V-shaped" instead of "U-shaped" in order to produce crimp with greater permanence. The processability characteristics of any fiber should make it possible, with a reasonable safety margh, to obtain the production rates and uniformity in opening, feeding, carding and other nonvoven or tacking processes proqued for efficiency and profitability.

An overall cohesion value of any given sample can be quickly determined by the cohesion-test method and instrument described in U.S. Patent 4,649,605 the disclosure of which is incorporated in its entirety herein by reference.

This method determines whether or not crimped staple (floors either natural or man-made, have a weighted-average cohesion number of from 5.6 to 12.5 inches (14.2 to 31.7 so enlimaters). This is done by initiating gas impringement contacts at successively-increasing different pressure levels against a carted web of staple filters to cause in the carted web the formation of visible budges until at least 90% of the budges are oventually ruptured for a particular pressure level. As such pressure, the ruptures form fails "bown upward by the gas imapingement which equal or exceed the height of a failure-indicator ber or photocell. The pressure and number of ruptures from each pressure level are recorded and a recipited-average cohesion number is determined therafrom. The standard sliver weight used in this tots is 65 grains per yard (4.61 grains per mater) but the instrument can be calibrated using other sliver weights. The laboratory is maintained at approximately 55% relative humidity at 75°F (24°C). The carding machine used for these leats had oquipment and settings which made it possible to produce at least generally acceptable card webs suitable for test purposes using filters with a wide denier-per-filtament range of about 1.1 to 7.0 (1.2 to 7.8 decitex) with staple lengths of about 1.25 to 2.0 3.2 to 5.1 million. The card was equipment and eventually an analyse left.

20 (a 2 to 3 cm) in each was equipped with an autoeverient.

Cotton has relatively low ochesion compared to that which can be obtained with certain well-crimped and properly lubricated man-made fibers. Therefore, whenever possible, man-made fibers should be lubricated and crimped so as a to exceed the ochesion level of cotton to a certain action in order to obtain high earding rates (in fibergame or pounds per hour) with at least satisfactory web and silver uniformity and strength. In view of the history of cotton, the ochesion-test instrument can be calibrated using a selected cotton to establish a desirable tange of cohesion values (above those of the selected cotton). For example, ochesion losts of a blended sample from a proporty-stored, aged bale of Memphies cotton with a Micronaire grade of 4 6 to 4.7 (standard test for grading octon) and an average staple length of 1 to 1.083 inches (2.6 to 2.7 cm) produced cohesion values of about 5.1 to 5.5 English (12.9 to 14 metric). A cohesion value is either on a comparative produced cohesion values of about 5.1 to 5.5 English (12.9 to 14 metric). A cohesion value is is either on an English or matric basis. Since it was known that this cotton was substantially typical incarding performance, the cohesion-test instrument was adjusted to provide cohesion values at the lower end of the cohesion-range. Thus, fibers with greater cohesiveness would be expected to provide cohesion values for comparison against other filber sample.

Tests for crimp frequency/angle and for % lubricant are important in starting and controlling the operation of a processing line but such information does not determine the fitness-tor-use of the filter interms of a comparative cohesion value. The cohesion value is helpful in this regard by providing a measure of comparative strength of the card web of one sample versus at least one other. In addition, the fiber mail fed to the card and the carded web are examined to determine how well the tibers have been escenarios.

Favorable comparative cohesion values and normal carding performance with excellent efficiency and production rates (kilograms or pounds carded por horuly can be obtained with our novel fibers, including the most-priorad caustic-treated non-round tibers produced by the nevel processes and hot-fubricant-application jets shown in Figures 1, 4, and 6

The determination of an approximate weight % lubricant on a fiber for minoral-oil-based lubricant is is made by the interared test method via analyses of the extract weshed from a sample of liber. Infrared absorption as described by Beer's Law is used to determine the mass of lubricant extracted into a suitable solvent, such as Frech (DuPort Corp.) The analyzer system dispenses solvent which washes the fiber to remove fubricant using a recirculating flow loop. The solution of French and lubricant is analyzed for total of the honds as it assess through an infranced absorption analyzer flow

cell, such as a Wilks-Miran IR analyzer. The resultant aignal is converted electronically to be displayed as the % bibricant (by weight). Conversion factors can be used to enable a single IR bibricant-lest instrument to be used for analysis of several different lubricants which have been applied to various types of fibers. For example, a single testing station could be employed 1) to enalyze polyseter fibers which have been tubricated appropriately for sewing thread, and 2) to sub-sequently analyze polysets fibers which received flubricant which is suitable for use in certain nomewore products. An IR lubricant-test instrument (the "Rothermel Finish Analyzer") can be purchased from Lawson-Hemphill Corp of Spartanburg, SC, USA.

Tube elution is the preferred method which can be used for determining the approximate weight % of hydrophilic lubricent such as the novel lubricent is or various libers. In this procedure, a methanol extraction is utilized to try to remove substantially all lubricent components from the flow, with a subsequent weighing to determine weight precretage lubricant. The tube elution method allows the determination of the amount of lubricant on a preveighed sample of floer by contracting the bulscent with methyl achord from the first sample which has been peaked into an open-medic glass tube. The alcohol is caught in an aluminum dish which is located on a steam bath. The alcohol is evaporated under controlled conditions, leaving the extracted lubricant as a residue. The weight of the residue is gravimetrically measured and the percent lubricant is calculated. Appropriate safety precautions must be tasken. These tests for weight 's lubricant are generally adequate but do have a certain amount of variability among laboratories, among operators, among repeat amples over time, set. Thus, it seems that it is not possible to measure exact or precise amounts of lubricant or any fiber. The process of the present invention provides flows could with a test one hydrophilic lubricant which provides improved overall performance, particularly when used within cortin weight? Kenages on certain fibers as described. The preferred minimum amounts of lubricant set forth in this specification should provide some margin for error in application and/or testina.

For the hydrophilic cellulose acetate fibers of Example 6, an approximate weight percent of the hydrophilic lubricant was determined substantially as described in ASTM Method D-2257-80 using diethylether in a Sohxlet extraction procedure.

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It is helpful to have an estimate of the differences in crimp characterizations such as crimp angle, crimp ratio, and crimp frequency of staple fibers. Crimp affects the carding of the fiber and the subsequent processing of the fiber indo a normworen fabric. Staple crimp can also affect the built, the hand and visual appearance of the finished product. The available test methods for crimp characterization must be used with caution as will be described. Crimp characterizations are important in helping to establish good operating conditions for crimpers and tow drivers. Such characterizations can help detect meior differences.

In this method of analyzing crimp, liber chip specimens of staple fiber are placed on a black plush surface. The crimps along the entire fiber length are counted. Both the relaxed (crimped) and extended fiber lengths are measured in inches or centimeters to one decimal place. The crimp angle and crimp ratio for each sample are then calculated

Crimp is defined as the waviness of a fiber, a deformation of a filament, or group of filaments, in either the vertical or horzontal plane to the longitudinal axis of the fiber, which is of repetitive nature and is intentionally induced in the fibers by use of external forces. Crimp level is defined as the number of angular peaks (crimps) per inn' of extended fiber length, noted as crimps per unit length. Crimp ratio is defined as the direct ratio of the relexad length of crimpsed fiber to the extended fiber length. A fiber chip is any group of crimpsed staple fibers (typically about 10 to 50) which remain in register after being out at the same time. Crimp angle is a calculated value obtained from the following formula:

Crimp Angle $\theta = 2 \text{ Sin}^{-1} \frac{\text{Relaxed Length}}{\text{Extended Fiber Length}}$

It is important that the limitations of the crimp frequency and crimp angle fests be understood. Not only are the abilities of these tests to predict "fitness-for-use" not satisfactory, the reproducibility and representativeness of practical samples sizes are not satisfactorily dependable. See ASTM Method D 9337 dated 1980 for the "Users and Significance" section in which severe limitations of the test method for crimp frequency are clearly stated. Also, see the "Applicable Documents" section in ASTM D 9337. This entire method is incorporated herein as a reference.

When it is desirable to prepare the various novel fibers without significant crimp, the crimper rolls can be used essentially as lorwarding rolls with no internal steam and with very low pressure applied by the clapper. As an alternative, squeeze rolls followed by appropriate forwarding rolls ("star" rolls) can be located immediately after the hot-lubricant iels to reclase the crimper.

The Automated Vertical Moiature Transport Test is one of the tests used herein to measure the vertical liquid transport capability of the fibers. The fibers are alther in original form or secured by how water plat as described and are placed made a placed to the control of the place of the

plastic tube of about 7 mm inside diameter and cutting the ends of the silver cleanly where they project from the 10.2 om tube), mounted, and the fluid is placed in contact with the bottom odge of the mounted specimen, the computer reads the balance (weight gain of the specimen) at predetermined intervals of time. Preparation of artificial perspiration is described in AATCC Test Method 15-1978. A graph of this data is then printed as shown in Figure 3.

As the number of suitable liquid transport grows in the fiber is increased, an increase in denire per filament tends to be needed to maintain the cross-section, spinning performance, production rates, the desired fiber quality and to aword broken filaments, etc. It is possible to obtain, through spinning and drawing combinations, fibers having final deniers of approximately 5.0 to 200 (5.6 to 222 decitox) per filament for the various fibers with about 5 to at least about 20 grows. However it is recognized that it could be no possible to proper a denient/filament loss than 5.0 (5.6 decitox).

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When treating the preferred non-round libers of the present invention with the hot processing lubricant solution it was unexpectedly found that excess liquid should be removed from the grooves of the fibers prior to contact with the hot solution containing processing lubricant. This is needed for fibers with 2 grooves but even more so to fibors with 8 or more grooves so that the lubricant solution can then flow into the grooves of the fibers. The location of this fliquid removal method can be as illustrated in Figure 1. Any method of effectively removing this excess liquid which is largely water can be considered to be useful within this preferred process of the present invention. However, contact bars, squeeze rolls and rigit sate preferred and an overel dyrings step is most preferred as shown after 2 in Figure 6. A charison to be used to judge the acceptability of an excess-liquid hardward system is whether or not the desired percent of lubricant and be applied to the tiber satisfactority after such excess liquid has been convoved and the novel controlled dying stop is most effective in this repard. Fibers with more than about two grooves such as a fiber with eight grooves (Figure 2d) array so much liquid (dilute acetic-acet solution) (arward to the crimper that the lubricant into mite jet is essentially indee on the surface of liquid and is not effective in the desired provided in the grooves to any important degree. The crimper then squeezes he well fiber causing most of the not furbricant and eventual liquid (week acetic-acid) solution to be removed, leaving the flow that ending the forms of the fiber of the fi

Two solutions to this residual liquid problem, with the second one representing the more preferred solution, are as follows:

(i) At least one air jet, such as those disclosed in U.S. Patents 3.458.890 and 3.786.574, could be equipped with an appropriate bood, return drain, set and used following the bars and/or soquears cells on the output ided of the neutralization bath (located as shown at 1 in Figure 1) to effectively reduce the level of residual solution on the fiber prior to reaching the not-lubricant jets and/or other application means for hot fubricant application prior to the crimpor (ii) A most prioritor diversalitip process permits the two to be substantially dried and/or basked following (1) neutralization, (2) an optional additional weahing treatment, (3) a liquid-removal step (such as bars and/or jets and/or squeeze rolls) and (4) an optional lubricant-application step. The fiber is then transported to receive the final application of hot lubricant prior to the crimpor. Soe Figure 6 for a drawing of this process which could offscilvely and efficiently apply high levels of the described lubricants to non-round fibers which have at least one growth.

Additionally, the novel hol-lubricant-jet (or jets) illustrated in Figure 6 can be used to apply lubricant(s) to tow in situations in which the causet treatment and subsequent neutralization steps are not used. This processes are be operated in a variety of ways in order to subject the selected fiber to various operating conditions, temperature(s), treatments, surface ocatins, but one solit processes and the surface ocatins, but one specified in a variety of ways in order to subject the selected fiber to various operating conditions, temperature(s), treatments, surface ocatins, but one specified in the surface ocatins, but one specified in the surface ocations, but one specified in the surface ocations, but one surface in the surface ocations.

Fibers with many well-formed grooves can contain more lubricant than those with few such grooves. Fibers with many grooves such as 8 or more preferably have at least about 0.3 wt % lubricant coated thereon, more preferably between about 0.5 and 2 wt. % of the novel lubricants applied to the surfaces and grooves thereof.

Cross-linking agents, such as epoxidized polyethers and polyglycityl ethers with suitable initiations, etc., can be applied using the improved processes to after the surface characteristics of the fifter or to modify the "hand" or feel, etc. The process shown in Figure 6 provides considerable flexibility. For example, it is possible to conveniently apply the solicited cross-linking agent and any initiator which may be needed at Jet (or Jets) 2A and subsequently apply a processing lubricant containing a minor amount of the cross-linking agent at Jet (or Jets) 2B, etc. Such cross-linking agents can contain a minor amount of ultraviolet (UV) inhibitors site.

This improved process (illustrated in Figure 6), has the capability to apply in a controlled manner, a variety of ulbricants and other materials to the selected tibers and to provide the appropriate heat treatments. Thus, versatifity is one of the major advantages of this improved process. As illustrated in Figure 6, it is preferred to cortact the fibers with at least a portion of the lubricant or a component of the lubricant (e.g. a solution containing polyethylene glycol 600 moncliurate alone) tollowed by heat-setting. This portion of the lubricant can be applied for example at 2 are between the 4th set of rols and the 2nd heat-setting unit. This application can then be followed by contacting the filters with heated lubricant at 2b. For crimped filters this is all preferably conducted prior to the crimper. However (as a novel but much less preferred process ulser the decrease illustrated in Figure 1, all each one heated component of a lubricant and/or a

cross-linking agent can be applied prior to the crimper; the tow is subsequently heat-set, and additional lubricant and/or other components can be applied by a conventional spray booth or brush applicator after the tow driver.

Relatively undrawn polysator binder fibers and amorphous copolysator binder fibers, etc. can be randored suitably pridrophilic by the application of a lessal 0.2% wis not lines 10.2% and most preferably at less 0.3 wt. % of the described heatering processing lubricants by the process of the present invention. Binder fiber can be blended with at least one other fiber or other material, such as wood pulp, and the blend is then heated to cause the binder fiber to bond with the other component, usually in a compressed statio, to make bonded non-woven hydrophilic products with various characteristics. A preferred copolysater binder fiber of about 2 to 8 denier filament (2.2 to 8.9 decitex) with a 1.5 or 2 inch (about 3.8 to 5.1 cm) staple length can be prepared from 100 mole % temphilialize acid, glive mole %, eithyrial gylocal and 3 mole %. 1.4-cy-cichoxanofimethanol. However, other binder fibers in cluding bicomponent types, can be used. Examples of suitable binder fibers and with CELBOND* sheathcote, proprietary bicomponent fiber made by Hachstram Chemical Company and "CELBOND* sheathcote, proprietary bicomponent fiber made by Hachstra Chemical Company and "CELBOND" sheathcote, proprietary bicomponent fiber made by Hachstram Chemical Company and the side-by-side bicomponent was and those made from polycleffine.

Rendering these fibers strongly hydrophilic provides a novel efficient meltood by which liquid-transport capability of the final products can be initiated or enhanced. A significant improvement in crimp formation can also be obtained if desired. In a typical application, these fibers are blended with at least one other fiber and subsequently bonded using heat and pressure. However, these novel pydrophilic copolyseter binder fibers also can be blended with wood pulp and/or other meltoralis to create products with enhanced overall fluight-inesport performance, including durability. When blended with wood pulp, etc., the copolyseter is usually cut to short staple lengths of about 0.6 inches (1.5 cm) or less and often contains reletative little or no crimo.

In rocent years, the supply of viscose reyon has diminished significantly. However, there are many excellent hydrophilic products containing this floer which have been developed overthe years, such as absorbent products, cleaning flabrics, filters, multi-purpose nonwovens, etc. The novel fibers of the present invention could be used to extend the supply of viscose reyor for walking an appropriate bland.

It is believed that high-strength, high quality fibers such as those used in polyester sewing-thread could also be benefited by treatment according to the process of the present invention.

The following examples are intended to further illustrate the invention and are not intended as a limitation thereon.

EXAMPLES

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Since fiber lubrication is not an "exact sclernoe", the identification above and in the following examples of a "poor," Lubricant from the processability standpoint does not mean it will automicativity cause a total processing inlaw on all nonwoven and textile equipment in all situations. However, it is believed that, overall, the poor lubricant, whether hydrophilition or otherwise, would cause significantly more problems, such as weak wabs and/or silver in carding, excessive wab breakthowns, holes in the webs and/or unower, olicularly whose, difficulty operating consistently at the desired high rate of production, unsatisfactory opening of the staple prior to carding, etc. On the other hand, a "good" lubricant does or automicationally process well on all equipment at all times under all conditions. Perhaps, in a given situation, he amount of this lubricant applied to the fiber might not be satisfactory or the fiber crimp could be poorly formed or too variable. There could be cases in which more of the lubricant is required in a particular process in order to perform well, etc. However, it is believed that, overall, this "good" lubricant would be more broadly applicable to a larger number of nonwoven and/or toxilip processes and onder processing conditions with more flowrobble results than the "good" that the standard of the processes and the processing conditions with more flowrobble results than the "good" that the standard processing conditions with more flowrobble results than the "good" that the standard processing conditions with more flowrobble results than the "good" that the process and the standard processing conditions with more flowrobble results than the "good" that the process and the processing conditions with more flowrobble results than the "good" the process and the processing conditions with more flowrobble results than the "good" the process and the process that the process of the process and the process and the process that the good that the process of the process and the proces

Example 1

The following example illustrates some deficiencies of crimped staple fiber samples that are not prepared according to the present invention. A sample of fiber tow having a "Figure 8" cross-section was prepared as follows:

Dried fiber-grade polyathylene tergothtalate (PET) polymer of 0.63 inherent viscosity (IV) was melt spun at about 29°C through a spinnerette having 824 holes of dumbboll ("Figure 6") shape. IV is the inherent viscosity as measured at 28°C at a polymer concentration of 0.50g/100 millilliors (Mi) in a suitable solvent such as a mixture of 60 weight % pinend and 40 weight % lottachloroebhane. The spun fibers of about 4.4 denier per filament (4.9 decitex per filament) (40f) were wound at 1250 molers per mirule.

Two samples of this polyester fiber ("Figure 8" cross-section) were prepared as drawn crimped staple with about 1.5 denier per filiament (1.7 declex per filiament) and 1.5-inch (38 cm) staple length using the process essentially as shown in Figure 1 except without the application of the hot lubricant by the jet prior to the crimper. Approximately 0.15 weight % and 0.3 weight % tubrocant was applied at room temperature by a spray method to the low after the low dryer.

The lubricant ("LUROL" 2617 from Goulston Co., Monroe, N.C.) consisted of methyl-capped POE (10) laurate as the major component and quatemary amine carbonate as the minor component. The components were dispersed in water to propare a 15% emulsion. The necessary guides were used to provide a path to and through the sprany to both.

and then to the cutter to cut the tow into staple. The weight % lubricant was measured by tube elution as previously described

The temperature of the first dirating bath with 2% acdium hydroxide solution was maintained at about 69°C. An overall draw ratio of about 3.3 was maintained during the drafting process. The heat-set unit was maintained at a temperature sufficient to produce a low temperature of about 140°C. After the heat-set unit, the fiber was neutralized with a weak (at least about 0.4 to 0.6% by weight) solution of acetic acid in water at about ocon temperature or above Contact bars were mounted on the downstream side of the neutralization bath in order to skim off a major portion of the liquid. The fiber was crimped and then heat-set at about 97°C for about 5 minutes after crimping, was lubricated and then cut into about 1.5 mch (3.8 cm) staple. These samples were run on a Research processing line using a lotal tow denier of about 50,000 to 80,000 (55.555 to 86.656 decitox). The tow had an average of 11 to 13 crimps per inch (about 4.3 to 5.1 crimps per cm) with approximately a 90-to-100 degree average crimp angle. The crimps per unit length and the crimp angle wow measured as previously described.

These two caustic-treated fiber samples had good liquid-transport capability but had variable crimp with relatively wide (open) crimp angles and poor cohesion values. Carded webs from various samples of this fiber tended to be weak with some unevan webs and/or web failures due to low cohesion.

Cohesion values for these fibers were determined by the instrument and method disclosed in U.S. Patent 4,649,605 as praviously described. The cohesion values for these fibers were low, avaraging about 4,005.0 (10.2 to 12.7 metric). As previously indicated, the cohesion number is introded to be used to indicate comparative cohesion of staple fibers. The cohesion values are determined during carding and indicate comparative strengths of card webs representing the various samples.

Example 2

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The purpose of this example is to illustrate the fiquid-transport performance of fibers prepared using various aspects of the present invention when compared to noninventive aspects. A number of samples were prepared and steat of or drop-wetting performance. The following conditions were used in this attudy using a Research processing line and about 55,000 (oat) for when first preformance. The following conditions were used in this attudy using a Research processing line and about 55,000 (oat) for when first 111 follat low decisity operated at a seesed of about 40 meters per minute.

- Polyester: Polyethylene terephthalate melt spun using the conditions essentially as described in Example 1 with spinnerettes for round and "Figure 8" cross-sections.
 - 2. Denier and staple length; about 1.5 x 1.45 inches (1.7 decitex x 3.7 cm)
 - 3 Fiber cross-sections: Round and "Figure 8" (One 180 kg creeling of undrawn fiber was spun for each cross-section.)
- Treatments: 2% caustic (C) followed by neutralization as described above and in U.S. Patent 4,842,792 or no caustic (N).
- Lubrication methods for the various samples: Two hot-lubricant jets (HIJ) located above the tow, as shown in Figure 4 placed within 30 inches (76 cm) of the crimper input using the process shown in Figure 1; prior-art lubrication after crimping (LAC); or no lubricant (NL).
- Lubricant target for all samples: 0.4+/-0.05 weight % using the same lubricant as used in Example 1.
- 40 7 Heat-setting treatment after crimping: 145+/-6°C for approximately 5 0 minutes with hot air circulation. Of course, the damp tow entering the dryer is not at this temperature for the entire time
 - Drop-wetting test method: AATCC 39-1971.
 - 9 Tow tensions after the tow dryer through the cutter for Samples A, B, D, F and G were maintained at the minimum that was consistent with good operation of the cutter. The minimum air flow necessary to transport the sizple from the cutter through the delivery system to the collection system was used. Tow tensions for the Samples C and E (lubricated after crimping) were higher at the cutter than the other samples because it was necessary to pass over the guides and rollers that guided the tow to and through the lubricant-spray booth prior to the cutter as shown in Figure 1. If was not necessary for samples A, B, D, F and C to pass through this booth.
 - 10. Norwoven fabric construction about 16 grams/sq yard (19.1 grams per eq, metar) of carded fiber was power-bonded with about 4 grams/sq yard (4.8 grams per sq, metar) of Eastbond 252 polyester powder. The batting was created in two layers from two norwoven carding machines located to deliver one layer on top of the other prior to the powder-application machine with subsequent heating and passage through bonding rolls to comprese the material to form a thin sheet of bonded norwoven fiber. This powder-bonding method is well known in the nonwoven manufacturing industry.
 - 11 Scouring method. Hot-water jet as described above. The jet delivered about 1100 cubic centimeters of water per minute which had been heated to about \$4^C \text{ with a pressure at the jet of 20 pet; (ISRPa) maintained at about 6 inches (15 centimeters) from the nonwoven samples (25 y XT.1. centimeters per sample) for 60 seconds.

Each sample of nonwoven fabric was tested for drop wetting in the original form and after receiving a 60-second scour. The average drop-wetting results (in seconds) are as set out in Table 2.

Table 2

10	Sample	Cross- Section	Ç∠N	HLJ/LAC	After Scour	Wetting Time *** Samples Were ed for: ec 60 Sec
	A.	Fig. 8	С	HLJ	2.8	4.3 to 7**
	в.	Fig. 8	N	HLJ	2.8	48
15	c.	Fig. 8	С	LAC	6.2	82
	D.	Round	С	HLJ	4.8	118
	E.	Round	С	LAC	7.6	600
20	F.	Round	N	HLJ	11.8	600
	G. *	Fig. 8	N	NL	600.0	600

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* A light water spray was necessary in order to process this unlubricated fiber through carding. The carding performance of Sample G was very poor and the resultant powder—bonded fabric was not uniform. Sample G does provide an indication of the large difference in the drop-wetting performance of unlubricated fiber compared to (1) non-round fiber (Sample C); (2) one embodiment of the novel fibers (Sample A); and (3) the other samples representing the various treatments shown above.

- ** Multiple tests were run on the scoured samples for the more preferred novel fiber.
- *** It is recognized that there is a certain amount of variability in the AATCC 39-1971 procedure caused by visual recognition and judgment of the end point at which the drop has been fully dispersed. To reduce variability, these tests were performed by one senior operator to make comparisons among samples as accurate as possible. Other operators could obtain differences in absolute time measurements due to the recognition and judgment factors.

The results were plotted graphically as shown in Figure 5 representing the wetting time in original condition and after scouring for 60 seconds.

The results for Sample F indicated that round cross-section filter processed without caustic but with the hot-lubricant jets to attempt to improve oring formation) had relatively poor liquid-transport durability. Unexpectedly, the results for Sample B indicate that, even without causate, the hot-lubrican-lej process followed by orimping and heat-soling as previously described could be of benefit in preparing products for at least one-time use (nonwovens for cleaning applications, wipes, incontinence products, etc.). The tests on Sample G, which was not lubricated with a hydrophilic product, did not produce satisfactory dron-vertion results.

In view of these overall results, our inventive process with less preferred lubricants provided drop wetting at least equal to and possibly somewhat better than the conventional processes.

Example 3

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Except for heat-setting at about 75°C instead of about 145°C, fiber essentially identical to Sample A in Example 2 was prepared using two hort-burbant lies located above the tow as shown in Figure 4. Approximately 0.4 weight % ubbrand was applied. This lubricant was applied. This lubricant was applied. This lubricant was applied. The foreign consisted of 70 weight % polyathylene glycol (80) monocleurate and 30 weight % polyoxyethylene (5) potassium leuryl phosphate prepared as 15 % emulsion in water. This sample had excellent wettability. However, when tested for cohesion during carding using the method previously described, the crimped staple sample had once (flow) cohesion and thus did not provide an exceptible belanced overall performance.

40 Example 4

Fiber-grade PET polymer of 0.64 IV was melt spun at 280°C through a 16-hole spinneratte to make filaments with "8-growe" cross-sections somewhat similar to that illustrated in Figure 2d. The 40 denier per filament fiber (44.4 decitex per filament) was spun at 1500 meters per minute and subsequently was processed on a tow-processing line as shown in Figure 1. The total tow denier was about 55.000 (61.111 decitex).

About 400 pounds (182 Kg) of this eight-groove fiber were spun and wound onto tubes in the relatively undrawn state; placed in the creed on the Research processing line; drafted with approximately 2-to-1 overall draw ratio in a heated bath containing 2% causelt to obtain about 20-22 denier per fillament (122 to 24.4 declav), processed through the sleam chest and heat-setting unit, immersed in the neutralization bath containing week acetic acid (about 0.5%), and treated with two top hot-bulicant jots in serios as shown in Figure 4 prior to the crimper and low dyer with the objective of obtaining at least about 0.4 to at least about 2% lubricant by weight dried onto the hydrolyzed fiber which was prepared in the form of crimped staple. See Figure 1 for a drawing of this process. The lubricant was the same type as was used in Examile 3.

Except for the necessary change in draw ratio, the processing conditions were similar to the ones used successfully on the "Figure 8" fiber as shown in the previous examples. However, the desired percent lubricant was not obtained. Surprisingly, two separate tests indicated that the lubricant level was only about 0.03 to 0.1 weight % using the same tube elution test that was used in the previous examples. After doubling the concentration of the lubricant supply from 20 to 40 weight %. In the fiber had now about 0.19 wt. Which was far body the most profered minimum and collection of

at least 0.5 wt. % or more for fibers with about 8 or more grooves. As the concentration of the lubricant supply was increased to 40 wt. %, the lubricant became thicker and difficult to work with, even when heated, and proper penetration into the tow band became increasingly difficult to achieve.

Moreover, with the jets fully open, there was a large loss of lubricant which poured over the sides of the tow into the lubricant drain. The crimper-roll pressure was then reduced to allow more lubricant to be carried forward with the tow, however, crimp formation deteriorated and was unacceptable.

We discovered that excessive liquid retention in the grooves was the problem. This excessive liquid simply blocked the lubricant from properly entering the grooves. A novel process was then designed to overcome this problem as illustrated in Figure 1 with at least one Partial Liquid Removal Means 1. In this case, in addition to the wiper bars that had been used for the "Figure 6" samples, an air-jet system was installed after the bars to remove the excessive liquid after the neutral pation bath and onto 1 to the hot-livitional ties.

Using this novel process with a concentration of about 25 wt. % of the fubricant in solution, fibers with eight grooves were prepared with at least 0.5 to 1.5 wt. % of the fubricant of Example 3 dried on in the tow driver as has been previously described. The fiber was found to be hydrophilic.

Example 5

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Caustic-treated fiber similar to that made for Sample A in Example 2 (except as stated below) was prepared using two hort-birdsend jets operated at about 60°C located above the tow as shown in Figure 4. The crimpol tow was dried in the tow dryer at 65°C for about 5 minutes. This example compares the fiber opening, carding performance, cohesion values and vartical-wicking performance of four hydrophilic birdinaris applied by hort-birdsent jets to 1.5 choins per filament, (1.7 clotic) per filament), 1.5 inch (35 cm), polyester fiber in a "Figure 6" cross-section. The fiber for all four lubricants was produced on the same line in an effort to hold processing variability to a minimum. The desired minimum weight % blorbeart was at least 0.3. The crimp froquency was approximately 14 to 16 crimpwind, 65 to 8 crimps per cm). The approximate mean crimp angle of about 70 degrees was obtained using the estimation method described in Example 8. However, as previously stated, crimp frequency and angle are useful roung statinates to have in satting up the operation of a processing line but are not sufficiently reproducible for acceptance sampling and do not provide an adequate indication of carding performance. Samples were treated as shown in Table 9.

		Wt. & Lubric
ple	Lubricant T Components By Wt. %	Test Performed On Crimped Staple Sample at the Cutter
_	90 PEG 600 Monolaurate 10 Antistat*	0.36
m	45 PEG 400 Monolaurate 45 PEG 600 Monolaurate 10 Antistat*	0.42
	90 PEG 400 Monolaurate 10 Antistat*	0.39
	Lubricant same as Example 1	0.32
* 4-ethyl,	4-ethyl, 4-cetyl, morpholinium ethosulfate	ate

The samples were made on a single processing line using the same crimper (34" width rolls) (1.91 cm) adjusted by the same oxperienced operators. The tests for % lubricant by weight (using tube outloin) indicated that at least 0.3 weight % had been applied to all samples by the two hot-blustenst jets (minimum had been mel). The tests that were made on the crimped staple sampled at the cutter during processing indicated an overall light grouping of results centering around an average of chould 7.3 weight? M. However, when the carded slever was tested later, it was found that, overall. Samples A. B and C had very good agreement as a group in average weight % lubricant but that Sample D was about 0.12 to 0.22 weight % lower than A. B and C. Samples D did exceed our minimum target of 0.3 wt. % in tests on both staple relative Each sample was placed in a chultefood system to be subsequently opponed by tumbling, spike aprox, fine opener

and air currents in the standard manner and then automatically fed to a textile carding machine which was equipped with a cohesion-test unit as described. The following results in Table 4 were reported by the Technical Service Laboratory personnel who conducted the valuations:

Table 4

	Sample	Fiber Opening Performance	Observation of Carded Web For Strength	Comparative Weighted-Average Cohesion Value
	Α	Good	Weak	4.6 (11.7 metric)
0	В	Good	Normal	5.7 (14.5 metric)
	С	Not Satisfactory	Normal	6.4 (16.3 metric)
	D	Good	Normal	5.6 (14.2 metric)

Overell no advantage was found for Sample D over Sample B. The tests and observations were made by experienced carding operators who have made many such tests on various types of polyster filters over a number of years. Thus, the results show that the bluenant formulation of Sample A provided good filter opening but poor orbinson while the formulation for Sample C did not provide satisfactory filter opening but did provide good cohesion. The results further indicate that when combined as was done for Sample B, the components provided good overall performance as shown above in addition, the results indicate that the proportions of the components of the lubricant used for Sample B could be varied to a certain extent to provide increased or decreased responses for different fibers and to satisfy different final objectives.

Carded silver (65 grains per yard, 46 grains per meter) from each of the four samples was saved for evaluation by the Auromated Vertical Moisture Transport Test previously described. Average capacity of each sample expressed as the weight of liquid per grain of filber (grains/grain) was as follows:

- Sample A 4.9
- Sample B 5 3
- Sample C 5.3

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Sample D - 4.2

The results are shown in Figure 3 and indicate that the novel 3-component lubricant (Sample B) is least as effective in vertical transport as the lubricants used for Samples A, C and D and possibly slightly more effective in this regard. The unexpected results indicate that the novel throe-component lubricant-antistat, particularly when applied in a heated condition by our novel jets, provides improved, well-belanced, overall performance and improved overall margn of safely in terms of fiber opening, ochesion, and processability with at least equal and possibly somewhat better hydrophilic performance compared to prior art. Additional versatility is indicated by favorable results obtained with different cross-sections and fiber polymers. The perferred application method is by our novel hot-lubricant jet process but other application mens can be considered.

Example 6

The purpose of this example is to illustrate the use of the present invention on fibers other than polyester Using the well known solvent-spinning process (acetone), cellulose acetate fibers of 3.3 derier per filament 3.67 decise) in a "Y-shapped" cross-section were spun from multiple cabinets and then were guided across a lubrisetting roll and link a crimper to form a 50.000 total denier crimped flow. This tow was then introduced under suitable low lension to the first soft rolls of the process shown in Figure 1. The tow was passed through a draw battle about 60 degrees 0 using a draw ratio of about 1.2 to 1.4 portion of this drawing step was used to remove the original crimp to create a low with little or no crimp for this exporiment. The bath was equipped with Liquid-Removal Means 1 on the output side and the low subsequently passed through a steam chest and the heat-setting unit both of which were maintained at about 100 degrees C. The bath and fliquid-removal means were also used to remove all least the most easily accessible portion of the sonnina lubriagent filmental of based).

A hot-lubricant jet applied the most preferred and novel hydrophilic lubricant (heated to 60°C) immediately prior to the 0.5-inch width crimpe (1.97 cm). The lubricant was composed of 4.9 m. % PEG 400 monolaurate. 4.9 mt. % PEG 600 monolaurate and 2 mt. % e-tethyl, 4-cellyl, morpholium ethosultate at a 20 mt. % concentration in water. These are the same three components used to prepare the lubricant for Sample B in Example 5 but with the antistat reduced to 2 mt. % with a corresponding increase in the other two components to 46% each. Approximately 0.75 mt. % of the lubricant was appointed to the fiber. The crimped tow was dried at about 70°C to about 5 minutes. The resultant stage had a

relatively dry hand

This test was intended to determine whether or not a relatively low level (for collubes excettab) of lubricant would be satisfactory for 1) processability on a nonwoven carding machine and 2) liquid-transport properties. The lowest satisfactory tension for cuttling a 2-inch staple (5.1 cm) length was used. The staple was found to have about 12 to 14 average crimps per rind, (4.7 to 5.5 crimps per cm) at about an 85 to 90 degree average crimp angle using the estimated method referribed in Example 8.

In a small-scale experiment, it was possible to card the fiber (on a carding machine for nonwovens) but there was no administration of statis at this weight '80 of the fubricant. Thus, it was clear that for production purposes, at least at the sight of the fubricant. Thus, it was clear that for production purposes at least at least the components of the fubricant would be needed for cellulose accusate fiber.

The carded web was then subjected to a needle-punching operation in order to create a nonwoven fabric which was suitable for testing. The needle-punched nonwoven weighed about 3.8 ounces per square yard (129 grams per square merely with a thickness of about 0.106 inches (0.27 cm) under a pressure of 0.01 pounds per square inch (0.059 kPa). The fabric had good liquid-transport properties as indicated by basket-sink tests in distilled water. The average basket-sink time was 5.98 seconds obtained from the following individual tests: 7.65.5 good and 3.00 seconds.

The cellulose acetate samples described in this Example 6 created a special analysis problem due to the fact that mineral-oi-based lubricant was applied during spinning and was only partially removed by the drafting bath prior to application of hostical dyrdcophic lubranal as subsequently described it was necessary to healt these samples for 16 hours at about 100°C in order to substantially remove the mineral oil before performing the tube-elution procedure. The draft samples were allowed to condition for about 8 hours to determine % moisture regain and were then dried at about 120°C for about 20 minutes criter to performing the tube elution procedure.

Example 7

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Fiber similar to Sample A in Example 2 was prepared using three hot-lubricant jets as illustrated in Figure 4. Approximately 0.4 to 0.5 weight % of the following lubricant was applied at a temperature of about 85 degrees C:

45 weight % PEG 400 monolaurate

45 weight % PEG 600 monolaurate

10 weight % 4-ethyl, 4-cetyl, morpholinium ethosulfate

The lubricated, crimped tow was heat-set at about 75°C in the tow dryer.

In order to properly seal off excess lubricant flow, it was helpful to cover the holes in the bottom jet which extended beyond the edges of the tow. These holes can be covered in any suitable manner, however, adjustable collars were used as shown in Figure 4. Then at least one bottom jet was oriented as shown to provent, as much as is practical, any dry contact between the jet surface and the tow. Preferably, the fiber-contact surfaces of the bottom jet are costed with a suitable long-warning material, such as a ceramic coating.

No problems were found in using the novel three-jet lubrication appearatus and method in this feat. Excessive flow was provided to the bottom jet with a return of excess lubricant to the lubricant heating and supply tank. Since three jets were not required to apply the target lubricant level to this about 55,000 to 60,000 denier tow (61,111 to 66,666 decitex) tow, the bottom jet was removed to continue the experimental work using the top two jets. The flow ress. "Figure 6" polyester of about 1.5 deniet per flament (1.7 decites per fillament) by about 1.5-inch (26 cm) steple length. We concluded that the novel three-jet design shown in Figure 4 would be of major benefit in applying heated lubricant to the larget tows of at least about 800,000 total denier (888,988 total decitex) up to several million total denier which are typical of full-scale production lines for polyester and other fibers.

Example 8

This example is a further illustration of the overall performance of the three-component lubricant-antistat composition used in Sample 8 in Example 5. An "Sprove" polyset filter drafted to about 5.9 denier per filament and crimble following application by jet of about 0.6 to 0.9 vt. % of this novel lubricant heated to about 0.6 eVp. The analyses of the vt. % lubricant on the fiber were 0.58 and 0.94 and represent two different tests conducted when the fiber was being run and then later sampled from storage. These results are further examples of variability that we have found at times in recent tests and also between Bloostpories, etc.

The crimped fiber was heated in the tow dryer at about 66 degrees for 5 minutes. The average crimp frequency was about 12 to 14 crimps per inch (4.7 to 5.5 crimps per cm) with a crimp angle estimated to be about 69 degrees.

The estimation method for crimp angle involves comparing lengths of crimped tow to the lengths obtained after straightening the same tow and converting the ratio of the lengths to an estimate of the average crimp angle

The staple was cut to about 1.5 inches (3.8 cm). It is important, particularly for non-round fibers such as illustrated in journess 2a, 2b, 2c and 2d to maintain the lowest tow tension entering the cutter that is consistent with satisfactory control of stable length in order to avoid zocessive increases in errim analle with a orduction in ordesion.

The textile carding machine used for this example was adjusted for running about 1.5 or less up to about 3.0 deinerificiament (1.7 or less up to about 3.3 decitex/filament) with the most satisfactory carding performance for these general multi-purpose settings. However, this carding machine was equipped and soft in such a manner that it was possible to run staple up to about 7.0 denierifilament 7.8 decitex per filament) with at least acceptable web formation even though this is outside that most satisfactory range. The 5.9 denierifilament (6 decitex) filament of the same carding machine equipped with a cohesion test instrument which was used for the other cohesion tests in order to obtain a weighted-average ochesion value to compare against the values obtained in Example 5. With the denierifilament outside the most satisfactory range, some undesirable belied-up and tangled fibers were produced between the carding cylinder and the fixed filate of the carding remember However, it was possible to produce an acceptable with for testing and a cohesion value of 5.6 (14.2 metric) was obtained. The verb was iguided to have at least adequate strength. Thus, the novel hot-buticant-jet process and novel three-component lutriciant-antistat could be used satisfactority for overall performance of the "Re-grovoe" (tips proviously described. The carded sitrer was found to be thyrochnic.

Example 9

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An "8-groove" polyester fiber was produced under the following conditions:

Drafting-bath temperature About 72°C

Liquid-removal means Contact bars and air jet Steam tube temperature About 185°C Caustic treatment None Neutralization treatment None Heat-setting rolls Not heated Crimper width 0.5 inches (1.27 cm) About 130°C (5 minutes) Tow-dryer temperature About 55,000 (61,111 decitex) Total tow denier About 12 to 14 (4.7 to 5.5 Crimp per inch 15 crimps per cm) Estimated crimp angle All samples were estimated by the tow-estimation to be greater than 90° 20 with the samples lubrimethod: cated by hot-lubricant jet having somewhat sharper 25 angles than spray-booth samples. Weight % lubricant applied* PEG 880 sorbitan 0.49 by jet (about 80-85°C) 30 monolaurate Same as a. 0.55 by spray (room b. temperature) 0.47 by jet (about 80-85°C) PEG 880 sorbitan monostearate 0.49 by spray (room d. Same as c. 4n temperature) *Each lubricant consisted of 98 wt. % of the major ingredient plus 2 wt. % 4-ethyl, 4-cetyl, morpholinium ethosulfate antistatic agent mixed as a 20 wt. % concentration in 80 wt. % water.

("8-groove" fiber) (11.1 +/- 0.6 decitex per filament) Staple length About 2 inches (5.1 cm)

Denier/filament

About 10 +/- 0.5

These fibers were subsequently bonded using Kodel 410 binder fiber as previously described to form an approximately 40-gram per square yard (48 grams per square meter) bonded nonwoven in which the fibers are heated and compressed to form the fabric in a manner well known in the art.

All four nonwovens were found to be hydrophilic in basket-sink and drop-wetting tests. This process in which the

tow diver was operated at 130°C was found to open tow crimp angles significantly wider than the angles obtained in Example 5 in which hot-lubricant application of the preferred bioricant formulations was used prior to crimping with the tow diver operational rises than about SBC See Example 5 for comparison in which the heat-setting rolls are heated and the tow dryer is operated at a temperature below about 85°C. The process illustrated in this Example 9 is less preferred than the process illustrated in Example 5 but can be used in those situations in which the resultant fiber is found to perform at least acceptable in the subsequent nonwoven and/or toxillic processing.

Example 10

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This example illustrates the application of the novel three-component fubricant-antistat composition used in Example 6 in an effort to attempt to create a hydrophile binder fiber. Kodel of 10 binder fiber (about 3 denien/fillement, 9 s) desictes per filament) [proviously described] was chosen. A relatively hydrophotic buhrcant (mineral-oil type) had been used satisfaction to this filter for a number of visars for various pronovern applications.

About 0.25 weight % of the lubricant of Example 6 was applied to the Kodel 410 binder (floor (about 3 denient/liament) y a spray booth at room temperature. Subsequently, this fiber was blended with a major portion (about 80 wt. %) of an "9-groove" ormoged staple. It was count that, during opening and feeding of the fiber, the binder (fiber had become brittle and broke into many small lengths. Laboratory testing revealed that this fiber had lost a significant amount of strength and % obrigation. Over a period of 50 days, the fiber became rapidly more brittle and wesker with sharply reduced elonation and is therefore on a cutted for this application as a binder float.

Example 11

This example illustrates the application of the two novel lubricants of Example 9 on separate samples and to attempt to provide a binder fiber with improved hydrophilic action. The lubricants used in Example 9 were applied at about 0.25 wt. % to samples of tow used to make Kodel 410 staple fiber. Over a period of 50 days, the tow samples had only slight losses of strength and elongation. Thus, these two lubricants would be satisfactory to use in preparing binder fiber with hydrophilic procepties.

Example 12

In an aging test of the novel three-component lubricant, hydrophillic, bonded nonwoven fabric of sample B in Example 5 were slored for over 7 months and were then examined. It was found that the bonded structure and hydrophillic function of these fabrics had been retained.

Claims

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- A process for treating fibers comprising:
- (A) contacting fibers in a tow band with a free flowing solution or emulsion containing about 5 weight percent or more of a non-tacky antistatic hydrophilic lubricant at a temperature between about 40°C and the boiling soint of the solution;
 - (B) spreading said solution or emulsion into said tow band to coat all surfaces of said fibers; and
 - (C) heating said fibers at a temperature of about 40°C or more for a sufficient time to dry the lubricant-coated fibers
 - wherein any excess liquid present in the fibers has been removed prior to said contacting of step (A) and said tow band coated with said solution is crimped or compressed after said contacting of step (A) but prior to said heating of step (C) and
 - wherein said lubricant either is comprising a mixture of high and low molecular weight polyethylene glycol fatty acid esters wherein the low molecular weight polyethylene glycol fatty acid ester has a molecular weight in the polyethylene glycol portion below 500 and the high molecular weight polyethylene glycol fatty acid ester has a molecular weight in the polyethylene glycol portion above 500
- is comprising at least one polyethylene glycol monolaurate or monostearate having a sorbitan group
- 2. The process according to Claim 1 wherein said lubricant also contains a minor portion of at least one compound

selected from the group consisting of coloring agents, aroma-enhancing agents, sorburing agents, anti-lungal agent anti-bacterial agents, defloamers, client hydrochilic components, bonding agents, mineral oils, acetic acid, critic acid, accorbs and, super-absorbert powders or polymers, fluorescent additives, antiseptic additives

The process according to claims 1 or 2 wherein said lubricant contains about 1 to 20 weight percent of an antistatic agent

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- 4. The process according to Claim 3 wherein said lubricant contains a minor portion of at least one antistatic agent selected from the group consisting of quaternary amine salts and salts of polyoxyethylene and organic faity alcohol esters.
 - 5. The process according to Claim 1 wherein said solution is an aqueous solution containing about 10 wt. % or more of said libricant and said fibers are contacted therewith at a temperature between about 50 and 100°C; said spreading in Step B is produced at least partially by crimper rolls, said heating in Step C is conducted at a temperature between about 40 and 135°C for at least 20 seconds; and said fibers are subsequently subjected to tension.
 - The process according to Claims 1, 2, 3, 4, or 5 wherein said fibers are selected from the group consisting of polyester, cellulose seter, modacrylic, rylion, viscoer rayon, and blends or mixtures thereof; have at least one axial groover, and are in the form of a tow of at least about 10,000 total denier (11,111 total decider).
 - 7. The process according to Claims 1, 2, 3, 4, 5, or 8 wherein said fibers provided to Step A are caustic-treated fibers that have between 2 and 30 said grooves which are substantially continuous and said fibers are contracted with said colution using at least one continuous flow means above said fibers and continuous flow means above said fibers and continuous flow means below said fibers and continuous flow means above said fibers and continuous flow means above said fibers.
 - The process according to Claim 1 wherein said fibers provided to Step A are substantially dry caustic-treated fibers that have at least one axial groove.
- The process according to Claims 1, 2, 3, 4, 5, 6, 7 or 8 wherein said fibers are hydrolyzed fibers having at least 1 groove and a denier per filament of about 0.8 to 200 (0.89 to 222 decilex) and said lubricant is an acueous solution containing at least 10 th. % of a mitute of high and low moticauls weight polyphyten glycol fattly acid esters and/or at least one polyethylene glycol fattly acid esters and/or as least one polyethylene glycol monolaurate or monostearate having a sorbitan group and, at least one agent selected from the group consisting of, an antistatic agent, a deloamer, an antiseptic agent, a cross-linking agent with or without a catalayta and an additive with bonding properties.
 - 10. The process according to Claim 9 wherein the low molecular weight polyethylene glycol fatty acid ester is polyethylene glycol fatty acid ester is polyethylene glycol fatty acid ester is polyethylene glycol foot monolaurate.
 - 11. A lubricant composition comprising a mixture of high and low molecular weight polyethylene glycol fatty acid esters wherein the low molecular weight polyethylene glycol fatty acid ester has a molecular weight in the polyethylene glycol fatty acid ester has a molecular weight polyethylene glycol fatty acid ester has a molecular weight in the polyethylene glycol fatty acid ester has a molecular weight in the polyethylene glycol fatty acid ester has a molecular weight in the polyethylene glycol fatty acid ester has a molecular weight in the polyethylene glycol portion above 500, wherein said lubricant also contains a minor portion of at least one compound selected from the group consisting of coloring agents, armanding agents, minoral ois, artiful rugal agents, armibacterial agents, debamens, other hydrophilic components, bonding agents, minoral ois, acotic acid, citic acid, ascorbic acid, super-absorbent powders or polymers, fluorescent additives, antiseptic additives, antiseptic additives, antiseptic additives, antiseptic additives, antiseptic additives.
- 50 12. The composition according to Claim 11 wherein said mixture contains a minor amount of an antistatic agent.
 - The composition according to Claim 12 wherein said antistatic agent is a salt of a quaternary ammonium compound or a quaternary amine compound.
- 14. The composition according to Claim 13 wherein said antistatic agent is 4-ethyl, 4-cetyl, morpholinium ethosulfate.
 - 15. The composition according to Claim 11 Wherein the low molecular weight polyethylene glycol fatty acid ester is polyethylene glycol 400 monolaurate and the high molecular weight polyethylene glycol fatty acid ester is polyeth-

ylene glycol 600 monolaurate.

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- 16. The composition according to Claim 15 wherein said mixture contains at least 40 weight % polyethylene glycol 400 monolaurate at least 40 weight % polyethylene glycol 600 monolaurate and up to 10 weight % 4-ethyl 4-cetyl, monoholiming ethosultate.
- 17. The composition of Claim 16 wherein the composition is in an aqueous solution.
- 18. A lubricant composition comprising a mixture of at least one polyethylene glycol monoleurate or monosterate having a sorbitan group and a minor portion of at least one compound selected from the group consisting of coloring agents, arms-unstancing agents, south-gast gents, anti-burget algents, anti-burget algents, deboamers, other hydrophilic components, bonding agents, mineral oils, acotic acid, cifric acid, ascorbic acid, super-rasorbort powders or polymers. Increasent additives, antibiotic additives antibiotic admisstrations.
- 19. The composition according to Claim 18 wherein said mixture contains a minor portion of at least one antistatic agent and a major portion of a lubricant selected from polyethylene glycol 860 sorbitan monolaurate, polyethylene glycol 880 sorbitan monosterate and mixtures thereof.
- 20. An article of manufacture comprising fibers, obtainable by the process according to any one of claims 1 10, having at least 1 groove, either caustic-treated or not caustic-treated, and having a denier per filament of 0 8 to 200 (9 89 to 222 deciex) selected from the group of fibers consisting of nytons, polyoleffins polyesters, cellulose esters, modacrylic, viscose rayon, and blends or mixtures thereof having 0.9 xt. % or more of at least one composition from claims 11, 12, 13, 14, 15, 16, 18, or 17 applied to their surfaces
- 25 21. An article of manufacture comprising binder fibers having about 0.3 wt. % or more of the lubricant from Claim 18 baked onto their surfaces
 - 22. An article of manufacture according to claim 20 wherein said fibers are formed into at least one component of a product selected from the group consisting of products containing at least one of said fibers in a blend with wood pulp, absorbent products, wiping-tiening webs or fabrics, insulation, aroma/flavor materials, lines, wicks, relatively thick battings, compressed bonded battings or webs, needle-punched battings or webs, bandages, incontinence products, filters, and combinations thereof.
 - 23. An article of manufacture according to claim 20 comprising continuous filaments, either crimped or not crimped, in tow form that have been subsequently opened or spread by rolls and/or jets, and are a part of nonwoven products or filters.
 - 24. An article of manufacture according to claim 20 comprising fibers having a cross-section that has at least two forf-shaped and or Y-shaped elements which are connected to a single central core element which can be solid or hollow which are joined at a central point so as to project outward therefrom, forming liquid-transport channels between said elements which also extend outward from the central point.
 - 25. An article of manufacture according to claim 24 comprising fibers having a cross-section of at least one opposing pair of fork-shaped or re-haped grows or channels and an opposing pair of the sibet-shaped dischaped deciments, all of which are joined at a central core so as to project outward therefrom forming liquid-transport channels between said elements which also oxtend outward from the central point.
 - 26. An article of manufacture according to claim 20 comprising fibers wherein at least one cross-linking agent has been applied to the surface thereof and cured prior to the application of at least 0.3 weight % of said composition.
 - 27. A process according to claim 1

(A) contacting heat-resistant (bors in a tow band with a free-flowing solution containing about 5 weight percent or more of a non-tacky antistatic hydrophilic lubricant containing a mixture of high and low molecular weight poylethylene glycol monolaurates at a temperature between about 40°C and the botting point of the solution wherein the low molecular weight polyethylene glycol monolaurate has a molecular weight in the polyethylene glycol portion below 50°C and the high molecular weight polyethylene glycol monolaurate has a molecular weight in the polyethylene oblocol potion above 50°C.

- (B) spreading said solution into said tow band to coat substantially all surfaces of said fibers, and (C) heating said fibers at a temperature of about 40°C or more for a sufficient time to dry the lubricant-coated fibers.
- 28. The process according to claim 27 wherein said spreading of step (B) is done at least partially by the driven rolls of a crimper and said fibers are crimped after said spreading of step (B) and prior to said heating of step (C).
 - 29. The process according to Claim 27 wherein the low molecular weight polyethylene glycol monolaurate is polyethylene glycol 400 monolaurate and the high molecular weight polyethylene glycol monolaurate is polyethylene glycol 600 monolaurate.
 - 30. The process according to Claim 29 wherein said mixture contains at least 40 weight % polyethylene glycol 400 monolaurate. I least 40 weight % polyethylene glycol 600 monolaurate. and up to 20 weight % 4-ethyl 4-cetyl, morpholinium ethosulfate.
 - 31. The process according to Claim 1 wherein said lubricant contains a major portion of a lubricant selected from the group consisting of polyethylene glycol 880 sorbitan monolaurate, polyethylene glycol 880 sorbitan monosaterate, and mixtures thereof and, a minor portion of all least one agent selected from the group consisting of, antisatic agent, a defoamer, an antiseptic agent, a cross-linking agent with or without a catalyst and an additive with bonding properties.
 - 32. A process according to Claim 1 for treating fibers comprising applying at least one cross-linking agent to said fibers prior to a crimping or compression means with subsequent curing on heated rolls or in an oven and at least 0.3 weight? so I non-tacky throthollic lubricant is applied after such curing means.

Patentansprüche

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- 1. Verfahren zur Behandlung von Fasem, umfassend:
 - (A) Inkontaktbringen der Fasen in einem Kabelband mit einer frei fließenden Lösung oder Emulsion, die etwa 5 Gew -% oder möhr eines nicht-klebrigen antalistischen hydrophilen Gleitmittels enthält, bei einer Temperatur zwischen etwa 40°C und dem Siedepunkt der Lösung,
 - (B) Verteilen der Lösung oder Emulsion auf das Kabelband, so daß alle Faseroberflächen bedeckt werden und (C) Enzeimung der Fasem auf eine Temperatur von etwa 40°C oder darüber für eine ausreichende Zeit, um die gleitmittelbeschichteten Fasem zu trockwen,
 - wobei beliebige, in den Fasem vorhandene Überschußflüssigkeit vor dem Inkontaktbringen in Schritt (A) entfernt wurde und das mit der Lösung beschichtete Kabelband nach dem Inkontaktbringen in Schritt (A), aber vor dem Erwähmen in Schritt (C), gekregot oder kompririer itwid und
 - wobei das Gleitmittel entweder eine Mischung aus Polyethylengykollettsäureestern mit hohem und niedngem Molekulargewicht umfaßt, wobei der Polyethylengykollettsäureester mit niedrigem Molekulargewicht ein Molekulargewicht im Polyethylengykolanteil von unterhalb 500 und der Polyethylengykollettsäureester mit hohem Molekulargewicht ein Molekulargewicht im Polyethylengykolanteil von oberhalb 500 hat,
- 45 oder mindestens ein Polyethylenglykol-Monolaurat oder -Monostearat mit einer Sorbitangruppe umfaßt
 - 2. Verfahren nach Anspruch 1. wobei das Gelimittel auch einen kleineren Anteile mindestens einer Vorbindung enthält, ausgewählt aus der Gruppe bestehend aus: F\u00e4rbungsmittel, aromasteigernde Mittel, Sp\u00fcmittel, Anfiplzmittel, anti-baktorreile Mittel, Ansichammttel, oder hydrophie Bestandtelle, Bindermittel, Minerakiole, Essigature, Zirnorensätre Ascorbins\u00e4ren, superabsorbierende Pulver oder Polymere, fluoreszierende Additive, antiseptische Additive, antistatische Mittel, Queverneutungsmittell und Mischungen dewon.
 - 3. Verfahren nach Anspruch 1 oder 2, wobei das Gleitmittel etwa 1 bis 20 Gew.-% eines antistatischen Mittels enthält.
- Verfahren nach Anspruch 3, wobei das Gleitmittel einen kleineren Anteil mindestens eines antistatischen Mittels enthält, ausgewählt aus der Gruppe bestehend aus: quaternäre Aminsalze und Polyoxyethylensalze und organische Fertatikoholester.

- 5. Verfahren nach Anspruch 1, wobei die Lösung eine w\u00e4\textruget steinge L\u00e4ce ung ist, die etwe 10 \u00e4ew \u00b3 \u00e5\u00e4ce der \u00e4\u00e4ce und 100^\u00b3 \u00e5\u00e4ce der \u00e4ce und etwe 50 und 100^\u00b3 Cin Kontakt gebracht werden; das Vertollen in Schrift (B) wird durch Krepwalzen zumindest feilweise bewirkt, das Erwarmen in Schnift (C) wird bei einer Terriperatur zwischen etwa 40 und 135^\u00f3 \u00fcb ber mindestens 20 Sekunden ausgel\u00fchrt und die Fasern werden im Anschluß daran mit Spannung beaufschliebt.
- Verfahren nach Anspruch 1, 2, 3, 4 oder 5, wobei die Fasern ausgewählt sind aus der Gruppe besiehend aus: Polyester, Cellulioseester, Modacryl, Nylon, Viskosefaserstoff und Blends oder Mischungen davon: diese haben middestens eine axiale Vertietlung und liegen als Kabel mit mindestens etwa 10,000 Derrier total (11.111 Dezitex total) vor.

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- 7. Vorfarhren nach Anspruch 1, 2, 3, 4, 5 oder 6, wobei die in Schrift (A) eingesetzten Fasem kaustisch behandelte Fasem sind, die zwischen 2 und 90 axiale Vertiefungen aufweisen, die im wesentlichen kontinuierlich verlaufen und wobei die Fasem mit der Lösung unter Einsatz mindestens eines kontinuierlichen Fließmittale so berhalb der Fasem und mindestens eines kontinuierlichen Fließmittals unterhalb der Fasem in Kontakt gebracht werden und die kontinuierlichen Filießmittals von angeordnet sind. 48g ein trockener Kontakt mit den Fasem vermieden wird.
- Verfahren nach Anspruch 1, wobei die in Schritt (A) eingesetzten Fasern im wesentlichen trockene kaustisch behandelte Fasern sind, die mindestens eine axiale Vertietung haben.
- 9. Verfahren nach einem der Ansprüche 1, 2, 3, 4, 5, 6, 7 oder 6, wobei die Fasem hydrolysierie Fasem eind mit mindestens einer Vertilefung und einem Denier pre Filament von etwa 0,8 bis 200 (0,89 bis 222 Dezitex), und vobei das Glatemitatel eine wäßings Lösung ist, die mindestens 10 Gew %- einer Mischung aus Polyethylenglykofettateureseten mit hohem und niedrigem Meliekultrigewicht und/oder mindestens ein Polyethylenglykol-Monolaurat oder –Monostearamt inlierer Schlategruppe und mindestens ein Mittel ausgewählt aus der Gruppe bestehen draus einem antisatischen Mittel, einem Antischaummttel, einem antisatischen Mittel, einem Ausgewählt aus der Gruppe bestehen dass einem antisatischen Mittel, einem Ausgewählt aus der Gruppe bestehen dass einem antisatischen Mittel, einem Ausgewählt und einem Gruppe bestehen dass einem Auftrage der Vertragen der Vertragen der Vertragen der Vertragen von der Vertrag
- Verlahren nach Anspruch 9, wobei der Polyethylenglykolfettsäureester mit niedrigem Molekulargewicht Polyethylenglykol-400-Monolaurat und der Polyethylenglykolfettsäureester mit hohem Molekulargewicht Polyethylenglykol-600-Monolaurat ist.
 - 11. Gleihmitelzusammensetzung, die eine Mischung aus Polyethylenglykoftetsäurestem von hohem und niedrigem Molekulargewicht umfallt, wobei der Polyethylenglykoftetsäurester mit niedrigem Molekulargewicht ein Molekulargewicht im Molekulargewicht im Molekulargewicht im Polyethylenglykolanteil oberhalb von 500 hat, und wobei das Gleithmitel auch einen kilenren Anteil mitdestens einer Velkondung ausgewäht aus der Gruppe bestehend aus Fahmitteln anden nien kilenren Anteil mitdestens einer Velkondung ausgewäht aus der Gruppe bestehend aus Fahmitteln and material handen highen der Anteilsauften der Velkondung hat der Velkondung hat der Velkondung hat der Velkondung hat der Velkondung von der
 - 12. Zusammensetzung nach Anspruch 11, wobei die Mischung eine kleinere Menge eines antistatischen Mittels enthält.
- 45 13. Zusammensetzung nach Anspruch 12, wobei das antistatische Mittel das Salz einer quatern\u00e4ren Ammoniumverbindung oder eine quatern\u00e4re Aminverbindung ist.
 - 14. Zusammensetzung nach Anspruch 13, wobei das antistatische Mittel 4-Ethyl-4-cetyl-morpholiniumethosulfat ist.
- 50 15. Zusammensetzung nach Anspruch 11, wobei der Polyethylenglykollfottsäureester mit niedrigem Molekulargewicht Polyethylenglykol-400-Monolaurat ist und der Polyethylenglykollfettsäureester mit hohem Molekulargewicht Polyethylenglykol-600-Monolaurat
- Zusammensetzung nach Anspruch 15, wobei die Mischung mindestens 40 Gew. % Polyethylengtykol-400-Monolaurat mindestens 40 Gew. % Polyethylengtykol-600-Monolaurat und bis zu 10 Gew. % 4-Ethyl-4-cetyl-morpholiniumethyauffal enthick.
 - 17. Zusammensetzung nach Anspruch 16, wobei die Zusammensetzung eine wäßrige Lösung ist

- 18. Gleimittetrussammensetzung aus einer Mischung von mindestens einem Polyethylenglyko-Monolaurat oder -Monostoarat mit einer Sofotilengruppen und niemen kleineren Anteil mindestens einer Verbindung ausgewählt aus der Gruppe bestehenda aus Einbernttel, aromasteigernde Mintel, Reinigungsenttel, Amptizmittel, antibaktereile Mitel, Anlisch-Aummittel andere Hydrophie Bestandelie. Bindenttel, Mineratöle, Essgäsierz. Zitroenseizer, Assorbinsäure. superabsorbierende Pulver oder Polymore, fluoroszierende Additive, antiseptische Additive, antistatische Mittel. Querventzurasmittel und Mischungen davon
- Zusammensetzung nach Anspruch 18, wobei die Mischung einen kleineren Anteil mindestens eines antistatischen Mittels und einen großeren Anteil eines Gleintrichs ausgewählt aus Polyethylenglykol-880-Sorbitammonolaurat, Polyethylenglykol-880-Sorbitammonostearat und Mischungen davon enthät.
- 20. Gegenstand aus Fasern, die nach einem Verfahren gemäß einem der Ansprüche 1 bis 10 erhältlich sind, mit mindestens einer Verfletung, entweder kauslisch berhandelt oder nichtkauslisch behandelt und mit einem Denler pro Filament von O. 8 bis 200 (9.8 bis 220 Dezitzuk, ausgewählt aus der Gruppe der Fasen bestehend aus: Nylons, Potycleline, Polyester, Zelluteseaster, Modacryflasern, Viskoselasern und Blends oder Mischungen davon mit 0,3 Gew. % oder mehr mindestens einer Zusammensetzung nach den Ansprüchen 11, 12, 13, 14, 15, 16. 18 oder 19, autoberzeht und deren Destüßerhen.
- Gegenstand umfassend Bindemittelfasern mit etwa 0,3 Gew.-% oder darüber eines Gleitmittels nach Anspruch 18, aufgebacken auf die Oberflächen.
 - 22. Gegenstand nach Anspruch 20, wobel die Fasem mindestens in einen Bestandteil des Produktes ausgeformt wurden, ausgewählt aus der Gruppe bestehend aus den Froutkten enthaltend mindestens eine der Fasen in einer Mischung mit hölzpulpe, Aberptionsprodukten, Wisch- und Reingungsgeweben oder Stoftbehnen. Diemstoff, Aroma- oder Geschmacksmateriallen, Überzugspapier, Dochte, relativ dicke Watte, komprimierte gebundene Watte oder Gewebe, nadelgeschlagene Watte oder Gewebe, Verbandstoffe, Inkoritinenzprodukte, Filter und Kombinationen davon.
- Gegenstand gemäß Anspruch 20, umfassend kontinuierliche Filamente, die entweder gekreppt oder nicht gekreppt sind, in Kabellorm das in der Folge durch Walzen und/oder Jets geöffnet oder gespleißt wurde, und die Teile eines nicht-gewobenen Produkts oder Filters sind.
 - 24. Gegenstand nach Anspruch 20, umfassend Fasern mit einem Ouerschnitt, der mindestens zwei gabelgestelige oder y-gestlige Elemente hat, die mit einem einzehen Zentralkernelement verknüpft sind, das fast oder hohl sein kann, und die mindestens an einem zontralen Punkt miteinender verknüpft sind, so daß sie nach außen gerichtet sind und Flüssigkieltstransportkanäte zwischen den Elementen, die sich ebenfalls nach außen gegenüber dem Zentralpunkt erstrecken, bilden.
 - 25. Gegenstand nach Anspruch 14, umfassend Fasern mit einem Querschnitt von mindestens einem sich gegenüberliegenden Paar aus Vertiefungen oder Kanâlen von gabelartiger oder y-artiger Gestalt und ein gegenüberliegendes Paar von schilitzariig ausgestaltoten Elementen, die alle an einem zontralen Korn vorkrüpft sind, so daß sie nach außen weisen und füssigkeitsfransportlerende Kanâle zwischen den Elementen, die ebenfalls von dem Zentralpunkt nach außen weisen, bilden.
- Gegenstand nach Anspruch 20, umfassend Fasern. wobei mindestens ein Quervernetzungsmittel auf die Oberfläche davon aufgebracht und vor dem Aufbringen von mindestens 0,3 Gew.-% der Zusammensetzung gehärtet wurde.
 - 27. Verfahren nach Anspruch 1, umfassend:

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(A) Inkortaktbringen einer wärmerssistenten Fasern in einem Kabelband mit einer freiffießenden Lösung, die etwa 5 Gew.-% oder darüber eines nicht-klebrigen antistatischen hydrophilen Gleitmittel enfrält, enthaltend inen Mischung aus Polyethylenghykei-Monoleural von hohem und niedrigem Molokulargewicht, bei einer Temperatur zwischen etwa 40°C und dem Siedepunkt der Lösung, webei das Polyethylenghykol-Monoleurat mit niedrigem Molokulargewicht ein Molokulargewicht im Polyethylenghykolei unterhalb von 500 und das Polyethylenghykol-Monoleurat mit hohem Molokulargewicht ein Molokulargewicht im Polyethylenghykol-Monoleurat mit hohem Molokulargewicht ein Molokulargewicht ein Molokulargewicht im Polyethylenghykol-Molokulargewicht ein Molokulargewicht im Polyethylenghykol-Molokulargewicht ein Molokulargewicht im Polyethylenghykol-Molokulargewicht ein Molokulargewicht ein Molokulargewicht ein Molokulargewicht in Polyethylenghykol-Molokulargewicht ein Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polyethylenghykol-Molokulargewicht ein Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polyethylenghykol-Molokulargewicht ein Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polyethylenghykol-Molokulargewicht in Polye

(B) Verteilen der Lösung auf das Kabelband, so daß dieses im wesentlichen auf allen Faseroberflächen beschichtet wird und

- (C) Erwärmen der Fasern auf eine Temperatur von etwa 40°C oder darüber für eine ausreichende Zeit, um die gleitmittelbeschichteten Fasern zu trocknen.
- Verlahren nach Anspruch 27, wobei das Ausbreiten in Schritt (B) zumindest teilweise durch die Antriebswalzen einer Kreppvorrichtung geschieht und die Fasem nach dem Verteilen in Schritt (B) und vor dem Erwärmen in Schritt (C) oekropot werden.
- Verfahren nach Anspruch 27, wobei das Polyethylenglykol-Monolaurat mit niedrigem Molekulargewicht Polyethylenglykol-400-Monolaurat ist und das Polyethylenglykol-Monolaurat mit hohem Molekulargewicht ist Polyethylen-chvkol-600-Monolaurat
 - Verlahren nach Anspruch 29, wobei die Mischung mindestens 40 Gew -% Polyethylengtykol-400-Monolaurat, mindestens 40 Gew. % Polyethylengtykol-600-Monolaurat und bis zu 20 Gew. -% 4-Ethyl-4-cetyl-morpholiniumethosulfat enthält.
- 31. Verfahren nach Anspruch 1. wobei das Gleilmittel einen größeren Anteil eines Gleitmittels, ausgewählt aus der Gruppe bestehend aus Polyerbylenglykol-850-Scribtlanmonotaurat, Polyerbylenglykol-850-Sorbitammonostearat und Mischungen und einen kleinen Anleit mindestens eines Mettles, ausgewählt aus der Gruppe bestehend aus; anlistalischen Mittel, Antischäummittel, antiseptischen Mittel, Quervernetzungsmittel mit oder ohne Katalysator und einem Additf vm Bil Diedeoinschaften, enthält.
- 32. Verfahren nach Anspruch 1 zur Behandlung von Fasem umfassend das Autbringen mindestens eines Quervernetzungsmittells unt die Fasem vor dem Kreppen der Kromprinieren und anschließendes H\u00e4nten ernermten Walzen oder in einem Olen und wobei mindestens 0,3 Gew. % eines nicht-klebrigen hydrophiten Gleitmittels nach dem H\u00e4ren ernermten bird.

Revendications

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- 30 1. Procédé de traitement de fibres comprenant :
 - (A) la mise en contact des fibres d'un câble de filature plat avec une solution ou une émulsion fluide contenant erviron 5% en poids ou plus d'un lubrifilant hydrophile antistatique non pégueux à une température comprise entre environ 40°C et le point d'ébullition de la solution;
 - (B) la dissémination de ladite solution ou émulsion dans ledit câble de filature plat pour enduire toutes les surfaces desdites fibres et
 - (C) le chauffage desdites fibres à une température d'environ 40°C ou plus pendant
 - une d'urée suffisante pour sécher les fibres enduites de lubrifiant, dans lequel tout excès de liquide présent clars les fibres a dé d'élimité avant liadite mise en contact de l'étage (A) et ledit d'âble de fisiture plat endruit de liadite solution est frisé ou comprimé après ladite mise en contact de l'étape (A) mais avant ledit chauffage de l'étape (C) et
 - dans lequel ledit lubrilliant comprend soit un mélange d'esters d'acides gras de polyéthylkneglycol de masse moléculaire élevée et taible dans lequel l'ester d'acide gras de polyéthylkneglycol de masse moléculaire lable au ne masse moléculaire dans la partie polyéthylkneglycol inférieure à 500 et l'ester d'acide gras de polyéthylkneglycol de masse moléculaire dans la partie polyéthylkneglycol supérieure à 500, soit au moins du mondeurate out du monséarate de polyéthylkneglycol supérieure à 500, soit au moins du mondeurate out du monséarate de polyéthylkneglycol présentant un grunoperment sorbitant parties.
 - 2. Procéde selon la revendicistion 1, dans loquel tedil librifiant contient également une petité portion d'au moins un composé sélectionné dans le groupe constitué par les colorants, les amplificateurs d'arôme, les nettoyants, les antitorigques, les antibactériens, les antimousses, d'autres composants hydrophiles, les achésifs, les huiles mini-rales, l'accide acédique, l'acide activité, parcide acédique, la propriet présent présent présent par les des distinctions de l'activité présent par l'activité par l'activité présent présent par l'activité présent par l'activ
- Procédé selon la revendication 1 ou 2, dans lequel ledit lubritiant contient environ 1 à 20% en poids d'antistatique.
 - Procédé selon la revendication 3, dans lequel ledit lubrifiant contient une petite portion d'au moins un antistatique sélectionné dans le groupe constitué par des sels d'amine quaternaire et des sels de polyoxyéthylène et d'esters

d'acide gras organique.

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- 5. Procédé adon la rovendication 1, dans loquel l'adite solution est une solution aqueuse contenant environ 10% en poids ou plus dudit l'abrifiant et lesdites fibres sont mises en contact avec celle-ci à une température comprise entre environ 50 et 100°C, ladité dissémination de l'étape B est produite au moins partiellement par des objindres frisours; ledit chauffage de l'étape C est réalisé à une température comprise entre environ 40 et 135°C pendant au moins 20 s, et lesdits fibres sont envise commise au traction.
- Procédé solon la revendication 1, 2, 3, 4 ou 5, dans loquel lasdities fibres sont sélectionnées dans le groupe constitué
 par le polysieur. l'ester de cellulose le modacrylique, le Nylon, la rayonne et leura mélanges; ont au moins une
 rainure axielle et ont la forme d'un câble d'au moins environ 10 000 deniers au total 111 til décite au total).
 - 7. Prodadé solon la revendication 1, 2, 3, 4, 5 ou 6, dans lequel lesdites fibres fournies à l'étape A sont dos fibres fraitées par un agent caustique, ayant entre 2 et 30 rainures axiales qui sont sensiblement continues et lesdites libres sont mises en contact avec ladite solution à l'aide d'au mons un moyen à écoulement continu au-dessus desdites fibres et au moins un moyen à écoulement continu en dessous desdites fibres, lesdits moyens à écoulement continu de dart osationnés de facon à éviter le contact à sea avec lesdites fibres.
 - Procédé selon la revendication 1, dans lequel lesdites fibres fournies à l'étape A sont des fibres traitées par un agent caustique, sensiblement sèches, qui ont au moins une rainure axiale.
 - 9. Procédé selon la revendication 1, 2, 3, 4, 5, 6, 7 ou 8, dans laquel lescites fibres sont des fibres hydrolysées ayant au mons une rainure et un titre par filament d'environ 0,8 à 200 deniers (0,89 à 220 décite), et lect it ubrifiant est une solution aqueues contenant au moins 10% en poids d'un mélange d'esters d'acides gras de polyétiny henglycol de masse moléculaire élevée et faible et/ou au moins d'u monolaurate ou monostéarate de polyétiny làneglycol ayant un groupement sorbitanne et au moins un agent sélectionné dans le groupe constituté par un antistatique, un anti-mousse, un afficient afficient avec voir sans catalveure ut un addifit avant des propriétés adhévies.
- Procédé selon la revendication 9, dans lequel l'ester d'acide gras de polyéthylèneglycol de masse moléculaire l'abble est du monolaurate de polyéthylèneglycol 400 et l'ester d'acide gras de polyéthylèneglycol de masse moléculaire élevés est du monolaurate de polyéthylèneglycol 600.
 - 11. Composition lubrillante comprenent un mélange d'esters d'acides gras de polyéthyleneglycol de masse moléculair elable, dans laqualle l'ester d'acide gras de polyéthyleneglycol de masse moléculair albie a une partie polyéthyleneglycol supérieure à 500, dans laqualle ladit lubrifiant contient également une petite portion d'au moins un composé sélectionné dans le groupe constitué par les colorants, les amplificatiours d'arbine, les nettoyants, les antiflongques, les antibaciériens. Les antimousses, d'autres composants hydrophiles, les adhésife, les huilles minérales, l'acide actique, l'acide accordibique, les poudres ou polymères superabsorbants, les additifs fluorescents, les additifs antiseptiques, les antistatiques, les récticulants et leurs mélanges.
 - Composition selon la revendication 11, dans laquelle ledit mélange contient une petite quantité d'un agent antistatique.
 - 13. Composition selon la revendication 12, dans laquelle ledit antistatique est un sel d'un composé ammonium quaternaire ou d'un composé amine quaternaire.
- Composition selon la revendication 13, dans laquelle ledit antistatique est de l'éthosulfate de 4-éthyl-4-cétylmorpholine.
 - Composition solon la revendication 11, dans laquelle fester d'acide gras de polyéthylèneglycol de masse moléculaire faible est du monolaurate de polyéthylèneglycol 400 et l'ester d'acide gras de polyéthylèneglycol de masse moléculaire élevée est du monolaurate de polyéthylèneglycol 600.
 - Composition selon la revendication 15, dans laquelle ledit métange contient au moins 40% en poids de monolaurate de polyéthylèneglycol 400, au moins 40% en poids de monolaurate de polyéthylèneglycol 600 et jusqu'à 10% en poids d'éthosulitate de 4-drivi4-destylmorpholine

- 17. Composition selon la revendication 16, la composition étant en solution aqueuse.
- 18. Composition lubrificant ocomprenant un mélange d'au moine du monolaurate ou monostévarate de polyéthy lèneglycol ayant un groupement sorbitanne et une petite portion d'au moins un composé sélectionné dans le groupe constitué par les colorants, les amplificateurs d'adrème, les nettévojents, les antificatiques, les antibactériens, les antimoussess, d'autres composants hydrophiles, les adhésifs, les hulles minérales, l'acide acétique, l'acide citrique, l'acide accobque, les poudres ou polymères superaboribants, les additis fluorescents, les additis antiseptiques, les antistatiques, les réfuciants et le une mélances.
- 19 19. Composition selon la revendication 18, dans laquelle lodit mélange contient une petite portion d'au moins un antistatique et une portion importante d'un lubritiant sélectionné parmi le monolaurate de polyéthylène glycol 850-sorbtanne. Le monostétarité de polyéthylène/polycel 850-obtanne et leure métanges.
 - 20. Article manufacturé comprenant des fibres qu'il est possible d'obtanir par le procédé selon l'une quelconque des revendications 1 à 10, sayant au moins une risurue, fraitées ou non traitées par un agent caustique et ayant un titre par filament de 0.8 à 200 deniers (0.89 à 222 décilex), sélectionnées dans le groupe de fibres constitué par les Nylons, les polycléfines, les polysetiers, les estres do cellibose, le modacry(lune, la rayonne a leurs métangas, ayant 0.3% en poiste ou plus d'au moins une composition selon les revendications 11, 12, 13, 14, 15, 16, 18 ou 19 anniunés aux l'eurs surfaces.
 - Article manufacturé comprenant des fibres liantes ayant environ 0,3% en poids ou plus de lubrifiant selon la revendication 18 cult sur leurs surfaces.
- - 23. Article manufacturé selon la revendication 20, comprenant des filaments continus, frisés ou non frisés, sous la forme de câbles de filature qui ont été ensuite ouverts ou étailés par des rouleaux et/ou des jets et font partie de non-tissée ou de filtres.
- 24. Article manufacturé selon la revendication 20. comprenant des fibres ayant une section transversale comportant au moins deux éléments en forme de fourche ou de Y, connectés à un élément noyau central unique qui peut être solide ou creux et joints en un point central de laçon à l'aire saitlie vers l'extérieur à partir de ce demins, formant des caraux de transport de liquide entre lesdits éléments qui s'étendent également vers l'extérieur à partir du point central.
 - 25. Article manufacturé selon la revendication 24, comprenant des fibres ayant une section transversale comportant au moins deux rainures ou canaux en forme de fourche ou de Y opposés et deux éléments en forme de lente opposés, qui sont tous réinuis à un noyau central de façon à faire saille wer le réclieur à pair de ce demis, formant des canaux de transport de liquide entre lesdits éléments qui s'étendent également vers l'extérieur à partir du point central.
 - 26. Article manufacturé selon la revendication 20, comprenant des fibres sur la surface desquelles a été appliqué et durci au moins un réticulant avant l'application d'au moins 0,3% en poids de ladite composition.
- 27. Procédé selon la revendication 1, comprenant

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(A) la mise on contact de fibres thermoréestantes d'un câble de fileture plat avec une solution fluide contenant environ 5% en poide ou plus d'un lubrifiant hydrophile antietatique non pégueux contenant un mélange de monoleurates de polyéthyèneglycol de masse moléculaire élevée et faible à une température comprise entre 40°C et le point d'ébuillion de la solution, dans laquelle le monoleurate de polyéthyèneglycol de masse moléculaire dans la partie polyéthyèneglycol inférieure à 50°0 et le monoleurate de polyéthyèneglycol de masse moléculaire élevée a une masse moléculaire dens la partie polyéthyèneglycol sudrieure à 80°0 et le monoleurate de polyéthyèneglycol de masse moléculaire élevée a une masse moléculaire dans la partie polyéthyèneglycol sudrieure à 80°0 et masse moléculaire élevée a une masse moléculaire dans la partie polyéthyèneglycol sudrieure à 80°0 et masse moléculaire élevée a une masse moléculaire dans la partie polyéthyèneglycol

- (B) la dissémination de ladite solution dans ledit câble de filature plat pour enduire sensiblement toutes les surfaces desdites fibres : et
- (C) le chauffage desdites fibres à une température d'environ 40°C ou plus pendant une durée suffisante pour sécher les fibres enduites de lubrifiant.
- 28. Procédé solon la revendication 27, dans lequel lacitle dissémination de l'étape (B) s'effectue au moins partiellement par les rouleaux menés d'un frisour et lesdites fibres sont frisées après ladite dissémination de l'étape (B) et avant lodit chauffanc de l'étape (C).
- 29. Procédé selon la revendication 27, dans loquel la monolaurate de polyéthylèneglycol de masse moléculaire faible est du monolaurate de polyéthylèneglycol 400 et le monolaurate de polyéthylèneglycol de masse moléculaire élevée est du monolaurate de polyéthylèneglycol 600

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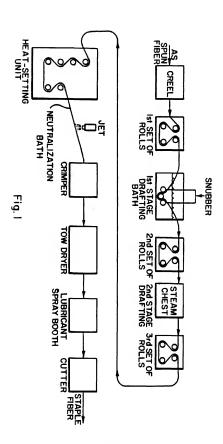
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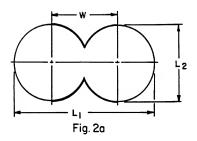
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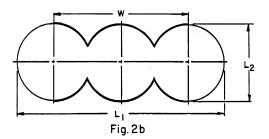
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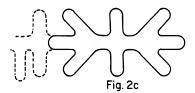
- Procédé solon la revendication 29, dans lequel ledit mélange contient au moins 40% en poids de monolaurate de polyéthyloneglycol 400, au moins 40% en poids de monolaurate de polyéthyloneglycol 600 et jusqu'à 20% en poids d'éthosultate de 4-éthyl-4-détylmorpholine.
 - 31. Procédé selon la rovendication 1, dans loque I lodit lubrifiant contient une portion importante d'un lubrifiant sélicationé dans le groupe constitué par le monolaurate de polyéthylèneglycol 890-sorbitanne, le monostéarate de polyéthylèneglycol 890-sorbitanne, le monostéarate de polyéthylèneglycol 890-sorbitanne et lieurs mélanges et une petite portion d'au moiss un agent sélectionné dans le groupe constitué par un antistatique, un antimousse, un antiseptique, un réticulant avec ou sans catalyseur et un additif ayant des propriétés achétèves.
- 32. Procédé solon la revendication 1 de traitement de liferes, comprenent l'application d'au moins un rétudient sur le lestites fibres avant un myord effisires un des compression neved utrissement unbeséquent sur des rouleaux charle. If so ou dans un four et l'application d'au moins 0,3% en poids d'un lubritient hydrophile non péqueux après lodit moven de durcissement.

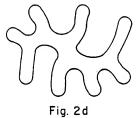


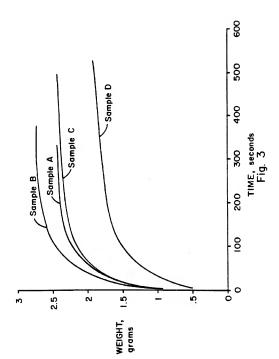
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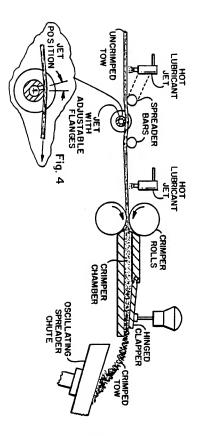




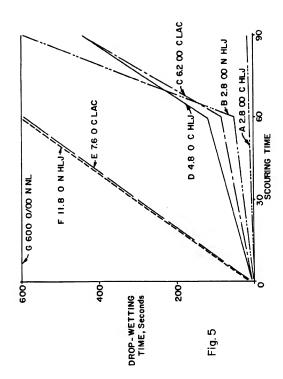


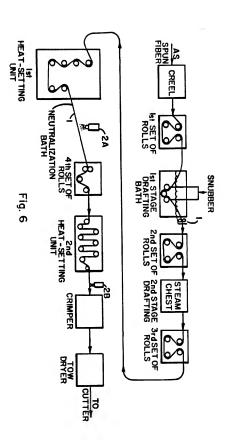






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